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Applicant: Ray W. Wood et al.

Title: METHODS OF ADMINISTERING LIQUID DROPLET AEROSOLS OF

NANOPARTICULATE DRUGS

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DECLARATION UNDER 37 C.F.R. §1.132

The undersigned, Gary G. Liversidge, hereby declares as follows:

I. Background of Gary G. Liversidge

- 1. I received my Ph.D. in 1981 from the University of Nottingham, England, in Pharmaceutical Chemistry. I have been working in the field of nanoparticulate drug technology since 1987, when I joined Eastman Pharmaceuticals.
- 2. Through a series of business transactions, Eastman Pharmaceuticals became Sterling Winthrop Pharmaceuticals Research Division, and then NanoSystems. This business then became known as the Elan Drug Technologies (EDT) business division of Elan Corp. PLC. EDT merged with Alkermes, Inc. on September 8, 2011 to form Alkermes, plc. Through a series of business transactions the current owner of the present application is Alkermes Pharma Ireland Limited.
- 3. Currently I am Chief Technology Officer and Vice President, R&D, at Alkermes plc, based at 852 Winter Street, Waltham, MA 02451.

II. Not all active agents can be formulated into stable nanoparticulate active agent compositions

- A. It is unpredictable whether a functional equivalent can be successfully made into a nanoparticulate active agent composition.
- 4. It is unpredictable whether a functional equivalent of a compound can be successfully made into a nanoparticulate active agent composition. This fact is demonstrated by the data below, detailing the successful preparation of a stable nanoparticulate cilostazol composition, in contrast to the unsuccessful attempts to make a stable nanoparticulate clopidogrel bisulphate composition. Clopidogrel is an inhibitor of platelet aggregation, and is a functional equivalent of cilostazol in inhibiting platelet aggregation.
 - (1) Stable nanoparticulate cilostazol composition was successfully obtained.
- 5. Cilostazol is a drug used to inhibit platelet aggregation. *See* abstract by Kimura et al., *Arzneimittelforschung*, 35(7A): 1144-1149 (1985) (Exhibit 1). Cilostazol is a poorly water soluble drug having an aqueous solubility of 3 μg/mL at 25°C or 6 μg/mL at 37°C.
- 6. As demonstrated by Jinno et al., *J. Controlled Release*, 111: 56-64 (2006) (Exhibit 2), a stable nanoparticulate cilostazol composition was successfully obtained by Elan's (now Alkermes') NanoCrystal[®] technology. *See* page 57, right column, section 2.3 for "Preparation of cilostazol suspensions." The obtained nanoparticulate cilostazol composition comprised hydroxypropyl cellulose and docusate sodium as the surface stabilizers. *Id.*, section 2.2 for "Particle size reduction of cilostazol." The nanoparticulate cilostazol composition had a median particle size of 0.22 μm (or 220 nm). *See* page 59, Figure 1, and section 3.1 for "Size distribution of milled cilostazol."
- 7. Exhibit 2 further demonstrates superior solubility, dissolution, bioavailability, and elimination of food effect for the nanoparticulate cilostazol composition in comparison to the

hammer-milled and jet-milled cilostazol compositions having a median particle size of 13 μ m and 2.4 μ m, respectively. See pages 59-63.

8. Accordingly, a nanoparticulate cilostazol composition was successfully obtained using NanoCrystal® technology, as demonstrated by the published scientific literature.

(2) Stable nanoparticulate clopidogrel bisulphate composition could not be obtained.

- 9. Clopidogrel is an inhibitor of platelet aggregation, and is a functional equivalent of cilostazol in inhibiting platelet aggregation. Clopidogrel bisulphate is insoluble in water at neutral pH but freely soluble in water at a pH of 1.0. Clopidogrel, as a methyl ester, is hydrolysed *in vivo* by esterases to an inactive carboxylic acid derivative, which represents more than 85% of the circulating drug related compounds in the plasma. Thus, only a small unknown portion of clopidogrel is available for metabolism to the active metabolite after oral administration. Therefore, it is highly desirable to obtain a stable nanoparticulate clopidogrel bisulphate composition to improve bioavailability of this drug.
- 10. The challenge in obtaining a stable nanoparticulate clopidogrel bisulphate composition is that during the milling process to reduce the particle size of clopidogrel, the pH of the milling mixture decreases while the dissolution of clopidogrel bisulphate increases. Accordingly, clopidogrel bisulphate undergoes auto-catalysis during the milling process until it is completely dissolved at pH 1-2. Solubilizing clopidogrel bisulphate does not solve the problem of poor bioavailability as *in vivo* the drug is hydrolysed by esterases to an inactive carboxylic acid derivative, as noted above.
- 11. Using the same NanoCrystal[®] technology, different approaches were attempted to stabilize particulate clopidogrel bisulphate during the milling process, such as milling in buffered systems and milling using the common ion effect, although none of these approaches resulted in a stable nanoparticulate clopidogrel bisulphate composition.

12. In a first set of experiments, milling of clopidogrel bisulphate was conducted in different buffered systems having a pH from 6.0-12.0 to prevent dissolution of clopidogrel bisulphate during milling. The results are detailed in the table below.

		Table 1		
Clopidogrel Bisulphate (% w/w)	Surface Stabilizer (% w/w)	Buffered System (pH)	pH prior to milling	pH post milling
5%	HPC-SL (2%)	93% w/w citric acid/sodium phosphate dibasic solution (pH 7.0)	not determined	2.21
5%	Plasdone S- 630 (2%)	93% w/w sodium phosphate monobasic/sodium phosphate dibasic solution (pH 8.0)	7.0	1.82
5%	Plasdone K29/K32 (2%)	93% w/w hydrochloric acid-Tris (hydroxymethyl) amino methane solution (pH 8.9)	2.0	Not milled due to dissolution of active agent prior to milling
5%	HPC-SL (2%)	93% w/w citric acid/sodium phosphate dibasic solution (pH 7.0)	6.0	2.17
5%	HPC-SL (2%)	93% w/w buffered solution (pH 12.0)	3.0	Not milled due to dissolution of active agent prior to milling
5%	Pharmacoat 603 (2%)	93% w/w simulated intestinal fluid (pH 12.0)	Not determined	2.0

- 13. Due to the dissolution of clopidogrel bisulphate in the buffered systems either prior to or post milling, despite the variable conditions attempted, it was found that it was *impossible* to obtain a stable nanoparticulate clopidogrel bisulphate compositions.
- 14. In a second set of experiments, milling of clopidogrel bisulphate was conducted under the condition of saturating the system with common ion, bisulfate ion, in a saturated

sodium bisulphate solution to control the equilibrium solubility of the clopidogrel during milling. The results are detailed in the table below.

***************************************	Table 2					
Clopidogrel Bisulphate (% w/w)	Surface Stabilizer (% w/w)	Observations				
5%	None	Microscopy showed the presence of drug particles in small quantities. The majority of material observed was in a flocculated state.				
5%	Pharmacoat 603 (HPMC) (1%)	After subsequent addition of stabilizer, flocculation appeared to be reduced but still present. An increased proportion of the drug appeared in the harvested aliquot suggesting increased milling of the drug. Brownian motion was not apparent.				
5%	HPC-SL (2%)	Some milled drug particles were apparent although in very small quantities. Particles did not exhibit Brownian motion. Flocculation was readily apparent throughout the aliquot of sample observed under microscope.				
5%	Tween 80 (2%)	Unmilled drug particles apparent. Aliquot harvested for microscopy was extremely dilute suggesting that very little drug was milled.				
5%	Pharmacoat 603 (HPMC) (2%)	Nanoparticles were observed in very small quantities. Particle did exhibit a small degree of Brownian motion.				
5%	Pharmacoat 603 (HPMC) (2%), DOSS (0.05%)	Very small quantities of milled drug particles were observed. Although particles were somewhat milled, they did not appear to be in the nanoparticulate size range. No Brownian motion was observed				
5%	Plasdone S-630 (2%)	Harvesting was not possible as the drug did not appear to mill. No microscopy was therefore performed. A large proportion of the slurry was observed on upper mill plate and agitator possibly leading to a void in the mill chamber reducing the milling efficiency.				
5%	Tyloxapol (1%)	Microscopy showed the presence of a very small concentration of milled particulates which appeared to exhibit Brownian motion most likely due to the diluted nature of the slurry.				

- 15. Despite the variable conditions attempted, it was found that it was *impossible* to obtain a stable nanoparticulate clopidogrel composition by controlling the equilibrium solubility of clopidogrel bisulphate via saturating the system with the common ion.
- 16. Accordingly, a stable nanoparticulate clopidogrel bisulphate composition could not be obtained using the NanoCrystal[®] technology under the various conditions tested.

B. Stable nanoparticulate or listat compositions could not be obtained.

- 17. Orlistat is a drug for treating obesity by preventing the absorption of fats from diet, thereby reducing caloric intake. However, orlistat is associated with significant gastrointestinal side effects, including steatorrhea, fecal incontinence, and frequent or urgent bowel movements. Therefore, it is desirable to obtain a nanoparticulate orlistat composition to alleviate the side effects.
- 18. The challenge in obtaining a stable nanoparticulate orlistat composition is that despite the attempts to mill approximately 30 different orlistat formulations, it was very challenging to obtain a nanoparticulate orlistat composition having the desired particle size due to a number of problems, such as difficulty encountered to "wet in" orlistat for milling, a significant quantity of unmilled orlistat remaining in the milling chamber, and difficulty encountered to harvest the milled orlistat.
- 19. Even when a nanoparticulate orlistat composition having the desired particle size was initially obtained, the composition was unstable under common storage conditions for a period of 14 days, as detailed in the table below.

		Table 3				
Formulation	Storage Time (days)	Storage Condition	Mean (nm)	D50 (nm)	D90 (nm)	D95 (nm)
Orlistat, 5%w/w	0	N/A	436	339	658	1009
Pharmacoat 603, 2%w/w	0	N/A	390	334	599	795

		Table 3				
Formulation	Storage Time (days)	Storage Condition	Mean (nm)	D50 (nm)	D90 (nm)	D95 (nm)
(Hydroxypropyl	14	5°C	50732	23999	139683	178902
methylcellulose) Deionised Water, 93%w/w	14	5°C	2045	362	7376	13593
Orlistat, 5%w/w	0	N/A	196	185	258	295
Pharmacoat 603, 1.25%w/w	0	N/A	195	185	257	294
(Hydroxypropyl	14	5°C	28076	196	100516	136455
methylcellulose) Lauryl Sulfate, 0.05%w/w	14	5°C	2439	208	8771	18960
(Sodium Lauryl Sulfate) Deionised Water, 93.7%w/w	14	25°C/60% RH	16072	170	72678	104171
Defonised water, 93.776w/w	14	25°C/60% RH	1214	212	717	7838
Orlistat, 5%w/w	0	N/A	649	296	1907	2925
Pluronic F108, 1.5%w/w	0	N/A	580	292	1487	2628
(Poloxamer 338)	14	5°C	38717	15805	106358	133797
Deionised Water, 93.5%w/w	14	5°C	314	164	286	693
Orlistat, 5%w/w	0	N/A	400	289	537	1017
Pharmacoat 603, 1.25%w/w	0	N/A	340	286	485	673
(Hydroxypropyl	14	5°C	64545	4924	209398	266403
methylcellulose) Lauryl Sulfate, 0.05%w/w	14	5°C	3405	311	12049	24135
(Sodium Lauryl Sulfate) Deionised Water, 93.7%w/w	14	25°C/60% RH	13556	189	58786	88122
Defonised water, 93.7% w/w	14	25°C/60% RH	814	211	984	3870
Orlistat, 5%w/w	0	N/A	176	164	225	261
Pluronic F108, 1.00%w/w	0	N/A	168	161	219	246
(Poloxamer 338) Tween 80, 1.00%w/w	14	5°C	1790	152	486	8500
(Polyoxyethylene Sorbitan Fatty	14	5°C	219	194	272	345
Acid Esters) Deionised Water, 93%w/w	14	25°C/60% RH	22241	371	90884	120263
2210111004 11 4101, 23 70111 11	14	25°C/60% RH	651	284	485	2949
Orlistat, 5%w/w	0	N/A	232	174	318	537
HPC-SL, 1.25%w/w	0	N/A	263	217	371	532
(Hydroxypropyl Cellulose-Super Low Viscosity) Docusate Sodium, 0.05%w/w (Docusate Sodium) Deionised Water, 93.7%w/w	14	5°C	40976	265	130336	174898
	14	5°C	3110	216	10063	22230
	14	25°C/60% RH	22255	170	84494	118656
	14	25°C/60% RH	506	192	302	2102
Orlistat, 5%w/w	0	N/A	419	330	639	971
HPC-SL, 2%w/w	0	N/A	438	331	671	1100

		Table 3				
Formulation	Storage Time (days)	Storage Condition	Mean (nm)	D50 (nm)	D90 (nm)	D95 (nm)
(Hydroxypropyl Cellulose-Super	14	5°C	76195	64261	175942	221539
Low Viscosity)	14	5°C	5418	399	19307	26735
Deionised Water, 93%w/w	14	25°C/60% RH	29931	19086	78580	96406
	14	25°C/60% RH	1211	310	3568	7161
Orlistat, 5%w/w	0	N/A	347	205	436	1330
Lutrol F127, 1.5%w/w	0	N/A	265	192	314	617
(Poloxamer 407) Deionised Water, 93.5%w/w	14	5°C	6161	167	24954	46361
Defonised water, 93.376w/w	14	5°C	219	192	271	344
Orlistat, 5%w/w	0	N/A	232	174	318	537
HPC-SL, 2%w/w	0	N/A	263	217	371	532
(Hydroxypropyl Cellulose-Super	14	5°C	40976	265	130336	174898
Low Viscosity) Deionised Water, 93%w/w	14	5°C	3110	216	10063	22230
	14	25°C/60% RH	22255	170	84494	118656
	14	25°C/60% RH	506	192	302	2102

20. Accordingly, a stable nanoparticulate or listat composition could not be obtained under the various conditions tested.

C. Banavath

- 21. The technologies employed to obtain nanoparticulate active agent compositions, such as precipitation, microemulsion, high pressure homogenization, and milling, are all associated with disadvantages. *See* Banavath et al., "Nanosuspension: An Attempt To Enhance Bioavailability Of Poorly Soluble Drugs," *Int'l J. Pharm. Sci. and Res.*, 1(9): 1-11 (2011) (Exhibit 3), at page 4, Table 2.
- 22. More specifically, precipitation may cause the growth of drug crystals and requires that the drug be soluble in at least one solvent. Microemulsion requires the use of a high amount of surfactant and stabilizer, which increases production cost. At times, microemulsion even involves the use of hazardous solvents in production. Homogenization requires that the

drug be pre-processed into a micronized state, and possible contamination may occur from metal ions from the wall of the homogenizer. Milling is a time-consuming process which is hard to scale up and which may have contamination from the milling media. Also prolonged milling may induce instability of the drug, resulting in the drug transforming into an amorphous state. Therefore, not all active agents can be successfully made into nanoparticulate active agent formulations in view of the technologies available to date.

D. Wu

- 23. Wu et al. ("Physical and chemical stability of drug nanoparticles," *Advanced Drug Delivery Reviews*, electronically published in February, 2011, Exhibit 4) report that it remains challenging to obtain nanoparticulate active agent compositions that are physically and chemically stable because the stability is affected by many factors. *See* lines 84-105 and 855-861.
- 24. More specifically, Wu et al. teach that obtaining a stable nanoparticulate active agent composition is hindered by the difficulty of selecting a suitable surface stabilizer for the active agent. Moreover, according to Wu et al. the main challenges in designing nanoparticulate drug formulations are: (i) the lack of a fundamental understanding of the interaction between the surface stabilizer and the active agent nanoparticles (see lines 268-273); (ii) the process of selecting a surface stabilizer having an appropriate anchoring tail to the particular active agent is burdensome (see lines 268-273); (iii) the lack of predictability due to the lack of any correlation between the physiochemical properties of the active agent and the success rate of obtaining a stable nanoparticulate active agent composition (see lines 399-402); and (iv) the lack of an efficient and high throughput screening technique to identify a suitable surface stabilizer (see lines 812-816).

CONCLUSION

- 25. The data described herein demonstrate unpredictability in the art, such that there is no *a priori* expectation that any given active agent could be made into a nanoparticulate active agent composition, even when a functional equivalent of the active agent has successfully been made into a nanoparticulate active agent composition. Therefore, it is impossible to predict whether a nanoparticulate active agent composition can be made based on the success in making nanoparticulate compositions of other active agents in the same class.
- 26. I declare that the statements made herein of my knowledge are true and all statements on information and belief are believed to be true; and further these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code, and that such willful false statements may jeopardize the validity of the application or any patent issuing therein.

Gary G. Liversidge

2/8/12

Date

Enclosures:

Publication by Kimura et al. (Exhibit 1);

Publication by Jinno et al. (Exhibit 2);

Publication by Banavath et al (Exhibit 3);

Publication by Wu et al. (Exhibit 4);

EXHIBIT 1

Display Settings: Abstract

Arzneimittelforschung. 1985;35(7A):1144-9.

Effect of cilostazol on platelet aggregation and experimental thrombosis.

Kimura Y, Tani T, Kanbe T, Watanabe K.

Abstract

A new antithrombotic drug, cilostazol (6-[4-(1-cyclohexyl-1 H-tetrazol-5-yl)butoxy]-3,4-dihydro-2(1H)-quinolinone, OPC-13013) was studied for its inhibitory effect on platelet aggregation in vitro in various experimental animals and man and in dogs ex vivo, for its effect to disperse platelet aggregates in vitro in rabbits and man and for its antithrombotic effect in vivo using its effect to prevent death due to the formation of pulmonary thrombi in mice. Cilostazol produced a potent inhibition of platelet aggregation both in vitro and ex vivo and a dispersion of platelet aggregates in vitro. The mode of action of cilostazol was different from that of acetylsalicylic acid (ASA) in that cilostazol inhibits not only secondary platelet aggregation but also primary platelet aggregation induced by aggregating agents such as adenosine diphosphate (ADP). The drug potently prevented death due to pulmonary thrombosis by platelet aggregates in mice in vivo. Unlike ASA which prevented only death due to collagen-induced platelet aggregation, cilostazol prevented both collagen- and ADP-induced platelet aggregation. These results suggest that cilostazol is a promising antithrombotic drug.

PMID:4074426[PubMed - indexed for MEDLINE]

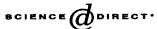
Publication Types, MeSH Terms, Substances

LinkOut - more resources

EXHIBIT 2



Available online at www.sciencedirect.com



Journal of Controlled Release 111 (2006) 56 - 64



Effect of particle size reduction on dissolution and oral absorption of a poorly water-soluble drug, cilostazol, in beagle dogs

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> Received 28 July 2005; accepted 22 November 2005 Available online 10 January 2006

Abstract

The purpose of the present study was to investigate the effects of particle size on the dissolution and oral absorption of cilostazol. Three types of suspensions having different particle size distributions were prepared of the hammer-milled, the jet-milled cilostazol crystals and the NanoCrystal spray-dried powder of cilostazol. In vitro dissolution rate of cilostazol was significantly increased by reducing the particle size. The dissolution curves of the cilostazol suspensions were in good agreement with the simulation based on the Noyes—Whitney equation. The bioavailability of cilostazol after oral administration to dogs was increased with reducing the particle size. While positive food effect on the absorption was observed for the suspensions made of the hammer-milled and the jet-milled crystals, no significant food effect was found for the suspension made of the NanoCrystal cilostazol spray-dried powder. These results could be qualitatively predicted from the in vitro dissolution data using the bio-relevant media, FaSSIF and FeSSIF. In conclusion, the NanoCrystal technology is found to be efficient to improve the oral bioavailability of cilostazol and to avoid the food effect on the absorption.

Keywords: Dissolution; Bioavailability; Particle size reduction; Food effect; NanoCrystal; Cilostazol

1. Introduction

Cilostazol is a synthetic antiplatelet agent with vasodialating effect [1]. This drug is approved for a treatment of ischemic symptoms related to peripheral arterial occlusive diseases in Japan and several other countries as Pletaal tablet, and for a treatment of intermittent claudication in U.S.A. and U.K. as Pletal tablet [2–5]. Recent study proved that cilostazol is also effective for a prevention of recurrence of cerebral infarction [6]. The molecular weight and melting point of cilostazol are 369.47 and 159.4–160.3 °C, respectively. Cilostazol is a neutral molecule having an aqueous solubility of 3 µg/mL at 25 °C [7]. Octanol—water distribution coefficients ($\log P_{\rm oct}$) of the drug ranged from 2.72 (pH 2.0) to 2.76 (pH 11.0) [7]. An apparent permeability of cilostazol through Caco-2 cell monolayer was found to be

 1.92×10^{-5} cm/s [8]. Therefore, according to Biopharmaceutics Classification System (BCS) [9], cilostazol is categorized in Class II (poorly soluble and highly permeable). Fraction dose absorbed of cilostazol from a suspension in 5% ethanol in rats or dogs was found to be 88.0% at 10 mg/kg or 50.7% at 3 mg/kg, respectively, calculated from the recovery of unabsorbed drug in feces [10,11]. The area under the serum concentration-time curve (AUC) of cilostazol for the 50 mg tablet was found to be significantly less (-13%) than that for ethanolic solution in humans. A shorter half-life $(t_{1/2z})$ of cilostazol at the apparent terminal elimination phase after dosing the ethanolic solution $(2.5\pm0.4 \text{ h})$ than that of the tablet (11.0±4.0 h) suggested that the absorption rate constant from the tablet was smaller than the elimination rate constant. These results suggest that the incomplete absorption of cilostazol from the tablet in humans was likely due to the poor dissolution [12].

It is well known that poorly water-soluble drugs often exhibit increased or accelerated absorption when they are

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administered with food [13]. This positive food effect would be attributed to the enhancement of the dissolution rate in the gastrointestinal (GI) tract caused by many factors such as delayed gastric emptying, increased bile secretion, larger volume of the gastric fluid, increased gastric pH (for acidic drugs) and/or increased splanchnic blood flow. In fact, a standard high fat breakfast increased both the rate (+91%) and extent (+24%) of cilostazol absorption after an oral administration of the 100 mg tablet [12], suggesting that the oral bioavailability of cilostazol could be enhanced due to the improvement of dissolution by food.

The dissolution rate of a solid drug can be expressed by the Noyes-Whitney equation [14], and it is also well known that the dissolution rate can be proportionally increased by increasing surface area as a consequence of comminution. Mechanical milling is a common technique to enhance dissolution of poorly water-soluble drugs [15]. Impact mills such as a hammer-mill or fluid energy mills such as a jet-mill are generally used for micronization of active ingredient in pharmaceutical industry [16]. In general, the former produces particles having mean diameters greater than 10 µm and the latter provides particles approximately ten times smaller than the hammer-milled particles. However, it is difficult to reduce particle size in sub-micron region using these dry-mills. NanoCrystal® is an enabling technology to produce submicron particles by wet-milling [17-19]. In this technology, materials are grinded with milling beads in water containing steric- and charge-stabilizers to prevent irreversible agglomeration of the resulted sub-micron particles. Anionic surfactants and hydrophilic polymers are used as the chargestabilizers and the steric-stabilizers, respectively. Significant enhancement of oral bioavailability by this technology was reported for some BCS Class II compounds [17,19]. Elimination of positive food effect was also reported as an advantage of NanoCrystal® [19].

The active ingredient of the commercial formulations is sized with a hammer-mill, resulting in mean particle diameter greater than 10 μm . Oral bioavailability of cilostazol, therefore, is thought to be improved by extensive particle size reduction with a jet-mill or a media-mill (NanoCrystal 60). The purpose of the present study was to investigate the effects of particle size on the dissolution rate as well as the rate and the extent of oral absorption of cilostazol. Food effect on the absorption was also investigated.

2. Materials and methods

2.1. Materials

Cilostazol and an internal standard OPC-13012 (6-[4-(1-cyclohexyl-I*H*-tetrazol-5-yl)propoxy]-3,4-dihydro-1-ethyl-2(1*H*)-quinolinone) were synthesized in Otsuka Pharmaceutical Co., Ltd. (Tokushima, Japan). Sodium taurocholate and egg lecithin (biochemistry grade) were obtained from Tokyo Kasei Kogyo Co., Ltd. (Tokyo, Japan) and Kanto Chemical (Tokyo), respectively. All other reagents were analytical grade commercial products.

2.2. Particle size reduction of cilostazol

The hammer-milled cilostazol crystal was prepared with Atomizer AIIW5G (Dalton, Tokyo) and the jet-milled cilostazol crystal was prepared with Super Sonic Jet Mill PJM-100SP (Nippon Pneumatic MFG Co., Ltd. Osaka, Japan). The NanoCrystal* cilostazol spray-dried powder, containing 16.5% of hydroxypropyl cellulose and 0.8% docusate sodium was prepared by spray drying of wet-milled cilostazol dispersion prepared with Dyno*-Mill (type KDL, Glen Mills, Inc., Clifton, NJ, USA). The NanoCrystal* cilostazol spray-dried powder exhibited excellent re-dispersibility in water, the simulated gastric and intestinal fluids in USP. X-ray diffraction analysis indicated that the crystal form of cilostazol was not changed by the milling procedures. No chemical degradation was found by the treatments.

Particle size distributions of the milled cilostazol crystals were determined with a laser diffraction particle size analyzer, SALD-3000J (Shimadzu, Kyoto, Japan), in 0.5% hydroxypropyl methylcellulose aqueous solution as a dispersing medium.

2.3. Preparation of cilostazol suspensions

The NanoCrystal[®] cilostazol suspension was prepared by dispersing the NanoCrystal[®] cilostazol spray-dried powder in water at 2.5 mg/mL. The hammer-milled and the jet-milled cilostazol suspensions were prepared with an aqueous solution containing hydroxypropyl cellulose and docusate sodium at the same contents of those in the NanoCrystal[®] suspension at the same concentrations.

2.4. Preparation of simulated intestinal fluids

The simulated intestinal fluids in the fasted state (FaSSIF) and the fed state (FeSSIF) [20] were utilized as dissolution media in order to predict in vivo dissolution and the food effect on cilostazol absorption. FaSSIF contains 3 mM sodium taurocholate and 0.75 mM lecithin, adjusted at pH 6.5. FeSSIF contains 15 mM sodium taurocholate and 3.75 mM lecithin, adjusted at pH 5.0.

2.5. Solubility measurement

Equilibrium solubility values of cilostazol at 37 °C were determined in water, FaSSIF and FeSSIF. Excess amount of the jet-milled cilostazol crystal was added in each medium in a screw-cap vial. Then, the vials were shaken continuously in a water bath maintained at 37 °C for 24 h. The equilibrated samples were immediately filtered through a 0.2 μm membrane filter, and the filtrate was diluted with appropriate volume of methanol. A 50- μL volume of the sample was analyzed by a reversed-phase HPLC method.

The solubility values of the hammer-milled cilostazol crystal and the NanoCrystal[®] cilostazol spray-dried powder were estimated from measured values of the jet-milled

crystal using the Ostwald-Freundlich equation [14,21,22] (Eq. (1)).

$$\ln \frac{C_{\rm s}}{C_{\rm s0}} = \frac{2\nu\gamma}{rRT} = \frac{2M\gamma}{\rho rRT} \tag{1}$$

where r, v, γ , R and T mean the radius of spherical drug particle, molar volume, interfacial energy, ideal gas constant and absolute temperature, respectively. ρ and M are the density and molecular weight, respectively. $C_{\rm s}$ is the solubility of the spherical particle, and $C_{\rm s0}$ is the solubility of a flat solid sheet.

2.6. In vitro dissolution profile measurement

In vitro dissolution profiles of the cilostazol suspensions were determined in 900 mL of water, FaSSIF and FeSSIF as dissolution media at 37 °C by USP Apparatus 2 using DT-610 dissolution tester (JASCO, Tokyo). Dissolved cilostazol was quantified from absorbance difference between the wavelengths of 257 nm and 325 nm. Based on the solubility values obtained in the previous section, 5 mg of cilostazol was applied as maximum amount to be solubilized in 900 mL of water. As a preliminary study showed that the dissolution profiles obtained at the speeds of 50 and 200 rpm were equivalent (data not shown), it was fixed at 50 rpm in this research.

2.7. Bioavailability studies in beagle dogs

Cilostazol was orally administered to four beagle dogs (body weight 8-10 kg) as the three types of oral suspensions, the hammer-milled, the jet-milled and the NanoCrystal® suspensions, at 100 mg/body in crossover design. A washout period of 1 week was kept between consecutive dosings. The dogs were fasted for 23 h before dosing and for 10 h post-dosing as a fasted condition. For the fed condition, the dogs were fasted for 22 h until 30 min prior to the dosing, and were then given 170 g of a solid food (CLEA Dog Diet CD-5M containing 24% protein and 9% fat, 635 kcal, CLEA JAPAN, Inc., Tokyo). The complete consumption of the food was ensured every time before dosing. Cilostazol dissolved in 5% DMSO was also intravenously administered to another group of four male beagle dogs (body weight 8-10 kg) at 10 mg/0.2 mL/kg. Dogs were allowed free access to water throughout the experiment. Blood samples (1.5 mL) were collected from a forearm vein with heparinized syringes at 0 (pre-dose), 0.5, 1, 2, 3, 4, 6, 8 and 10 h post-dose for the oral administration and 0 (pre-dose), 0.5, 1, 2, 5, 15, 30, 60 and 120 min postdose for the intravenous administration. Serum samples were obtained by centrifugation of the blood samples and stored at -20 °C until use. Our investigations were performed after approval by our local ethical committee at Otsuka Pharmaceutical Co. Ltd. and Okayama University and in accordance with "Principles of Laboratory Animal Care" (NIH Publication # 85 - 23).

2.8. Analytical method

2.8.1. Cilostazol in the simulated intestinal fluids

Samples of solubility measurement were introduced onto an HPLC system, consisting of an HPLC pump (Model LC-10A, Shimadzu, Kyoto) and a UV detector (Model SPD-10A, Shimadzu) set at 254 nm. A C18 column (TSK gel ODS-80Ts, 4.6 mm i.d. × 150 mm, Tosoh, Tokyo) was used as an analytical column. A mobile phase containing 0.2% w/v sodium lauryl sulfate and 0.03% v/v phosphoric acid in acetonitrile—methanol—water mixture (3:3:4, v/v/v) was delivered at 1.0 mL/min. Coefficient of variation of standard curve ranged from 0.24% to 1.15% and the correlation coefficient was over 0.999.

2.8.2. Cilostazol in serum

Cilostazol in serum was determined by validated HPLC methods using OPC-13012 as an internal standard. A 200 μL volume of the internal standard solution (1 µg/mL in acetonitrile) was added to a 200 µL volume of the serum sample diluted with blank serum if it was needed. Then it was mixed well with a vortex mixer and stood for 20 min at the room temperature. A 200 μL volume of water was added to the mixture and mixed well with the vortex mixer. The mixture was centrifuged at $1800 \times g$ for 10 min, then the supernatant was filtered through a 0.45-µm membrane filter. The samples were applied to an HPLC system, consisting of an HPLC pump (Model Nanospace 3001, Shiseido, Tokyo) and a UV detector (Model Nanospace 3023, Shiseido) set at 254 nm. A 100 μL of the resulting filtrate was injected to the pre-column, TSK precolumn BSA-ODS (4.6 mm i.d. \times 10 mm, Tosoh), adjusted at 40 °C and the pre-column was washed with the mobile phase for purification (1:10 diluted phosphate-buffered saline (-)) for 2 min at the flow rate of 500 µL/min, then it was back flushed to the analysis column, Capcell Pak C18 MG S-3 µm (3.0 mm i.d. × 75 mm, Shiseido) adjusted at 40 °C with the mobile phase for analysis (a mixture of acetonitrile-water (2:3 v/v) containing 0.3% v/v of THF) for 5 min at 300 µL/min. The chromatograms were obtained at the detection wavelength of 254 nm. Calibration curves (10-1000 ng/mL, 10 concentrations) and quality control (QC) samples (20, 200 and 1000 ng/ mL) were freshly prepared for each analysis. The lower limit of quantification by this method was 10 ng/mL. The linear regression coefficients of the calibration curves ranged from 0.99 to 0.9999. The accuracy and the precision of the QC samples ranged from 92.0% to 118.0% from the nominal values, and 2.3% to 14.5% CV, respectively. Several samples were assayed by using the HPLC system, consisting of the HPLC pump (Model LC-10A, Shimadzu) and the UV detector (Model SPD-10A, Shimadzu) set at 254 nm. TSK precolumn BSA-ODS (4.6 mm i.d. \times 35 mm, Tosoh) and YMC AM-302 S-5 μ m (4.6 mm i.d. \times 150 mm, YMC, Kyoto) were used as a pre-column and an analytical column, respectively. The linear regression coefficients of the calibration curves (10-1000 ng/ mL) were higher than 0.9999. The accuracy and the precision of the QC samples ranged from 96.4% to 109.0% from the nominal values, and 0.7% to 5.8% CV, respectively.

2.9. Pharmacokinetic analysis

The highest serum concentration of cilostazol was employed as $C_{\rm max}$, and the time to reach $C_{\rm max}$ was defined as $t_{\rm max}$. AUC and the area under the first-moment curve, AUMC, were calculated from 0 to infinity using a linear trapezoidal rule. The serum concentration at time zero (C_0) for intravenous administration was estimated by extrapolation. The mean residence time, MRT, was calculated by AUMC/AUC. The absolute bioavailability (F) was calculated based on Eq. (2).

$$F = \frac{AUC_{oral}}{AUC_{i.v.}} \times \frac{Dose_{i.v.}}{Dose_{oral}}$$
 (2)

where AUC_{oral} and Dose_{oral} are AUC at infinite time and dose for oral administration of cilostazol. AUC_{i.v.} and Dose_{i.v.} mean AUC and dose for intravenous administration of cilostazol.

The in vivo absorption rate of cilostazol was estimated using a numerical deconvolution technique. The mean serum concentration data from the oral administration study were assigned as a response function, while the data from the intravenous administration study were used as a weight function.

2.10. Simulation of in vitro dissolution

In vitro dissolution of the cilostazol suspensions was simulated by the method reported by Hints and Johnson [23], where they expanded a mixing tank model for monodispersed solid drug [24] to polydispersed particles [23,25,26]. Assuming that spherical particles have size fractions i=1 to n, that the number of particles dose not change with time and that the diffusion layer thickness at time t is equal to the particle radius at time t, the rate of change in the mass of remaining solid of the particle size fraction t is given by Eq. (3):

$$\frac{\mathrm{d}X_{s_i}}{\mathrm{d}t} = -\frac{3\mathrm{D}X_{0_i}^{2/3}X_{s_i}^{1/3}}{\rho r_0^2} \left(C_{\mathrm{s}} - \frac{X_{\mathrm{dT}}}{V}\right)$$
(3)

where X_0 is the initial mass of the drug, X_{si} is the mass of the remaining solid drug at time t for size fraction i. $X_{\rm dT}$ is the total mass of the dissolved drug at time t for the size fractions i=1 to n. D and ρ mean the drug diffusivity in aqueous phase and the density of the drug, respectively. r_{0i} is the initial particle radius of particle size for fraction i. C_s and V are the solubility of the drug and fluid volume, respectively. The rate of change in the mass of dissolved drug is given by Eq. (4).

$$\frac{\mathrm{d}X_{d_{i}}}{\mathrm{d}t} = \frac{3\mathrm{D}X_{0_{i}}^{2/3}X_{s_{i}}^{1/3}}{\rho r_{0_{i}}^{2}} \left(C_{s} - \frac{X_{\mathrm{dT}}}{V}\right) \tag{4}$$

where X_{d_i} represents the mass of dissolved drug for size i at any time.

The total masses of the remaining solid drug, X_{sT} , and dissolved drug, X_{dT} , at time t for the size fractions i=1 to n were described by Eqs. (5) and (6), respectively.

$$X_{\rm sT} = \sum_{i=1}^{n} X_{\rm s_i} \tag{5}$$

$$X_{\rm dT} = \sum_{i=1}^{n} X_{\rm d_i} \tag{6}$$

 $X_{\rm sT}$ and $X_{\rm dT}$ were simulated from Eqs. (3)–(6) by the 4th Runge–Kutta numerical integration method using a computer software, Mathematica 5.0 (Wolfram Research Inc., Champaign, IL, USA). The true density of cilostazol was determined with a gas pycnometer, Accupyc 1330 (Micromeritics, Norcross, GA, USA). The diffusivity of cilostazol in water was estimated by a method reported by Hyduk and Laudie [27] using a molar volume estimated by Schroeder's method [28].

2.11. Statistical analysis

Statistical analysis of the effects of particle size and food were performed by Welch's test using PSAG-CP® software (ASmedica, Osaka). *P*-value less than 0.05 was considered significant.

3. Results and discussion

3.1. Size distribution of milled cilostazol

Particle sizes of the three different types of milled cilostazol were measured and the size distributions are shown in Fig. 1. The median particle diameters of cilostazol in the hammermilled, the jet-milled and the NanoCrystal[®] suspensions were found to be 13, 2.4 and 0.22 μm, respectively.

3.2. Solubility

Equilibrium solubility values of the jet-milled cilostazol crystal at 37 °C were determined to be 6.26 ± 0.06 , 6.35 ± 0.12 and $12.7\pm0.2~\mu g/mL$ in water, FaSSIF and FeSSIF, respectively. The solubility in FeSSIF superior to that in FaSSIF or water could be attributed not to pH but to micellar solubilization due to higher concentration of sodium taurocholate and lecithin, since cilostazol is a neutral lipophilic compound. The solubility values of the hammer-milled cilostazol crystal and the NanoCrystal cilostazol spray-dried powder were estimated to be practically identical (0.4% less) and 6% greater than those of the jet-milled cilostazol crystal, respectively. The parameters

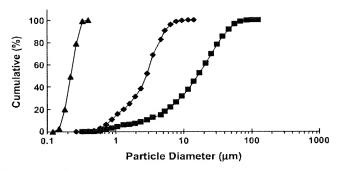


Fig. 1. Particle size distribution of cilostazol suspensions. Keys: ▲, NanoCrystal® spray-dried powder; ♦, jet-milled crystal; ■, hammer-milled crystal.

Table 1
Parameters for dissolution simulation

Parameter	Value
X_0 : initial dose	5 mg
C _s : solubility ^a	6.26 μg/mL (in water)
	6.35 μg/mL (in FaSSIF)
	12.7 µg/mL (in FeSSIF)
$D_{\rm eff}$ diffusivity	$4.04 \times 10^{-4} \text{ cm}^2/\text{min}$
ρ : density	1.26 g/cm^3
V: fluid volume	900 mL
Integration step	0.1 min ^b
	0.01 min ^c

^a For the hammer-milled and the NanoCrystal[®] suspension, these values were multiplied by 0.996 and 1.06, respectively, according to the Ostwald– Freundlich equation.

used for this calculation are as follows: M=369.47 g/mol, $\gamma=30$ mN/m, $\rho=1.26$ g/cm³, $R=8.314\times10^7$ g cm²/s²/K/mol, T=310 K [22].

3.3. In vitro dissolution rate

In vitro dissolution of cilostazol from the suspension consisting of the hammer-milled, the jet-milled crystals or the NanoCrystal cilostazol spray-dried powder was investigated in water and the bio-relevant media, FeSSIF and FaSSIF. Solubility of cilostazol in these media is not enough to solubilize clinical doses (50 mg or 100 mg) in 900 mL as shown in the solubility study. Therefore, 5 mg of cilostazol was applied as maximum amount to be solubilized in 900 mL of water, FeSSIF or FaSSIF. Furthermore, the simulation method was also employed to assess the dissolution of cilostazol from the suspensions. The parameters used for the simulation are listed in Table 1. Results shown in Fig. 1 were used as data of particle size distribution. Solubility values obtained in the previous section were also used for the simulation.

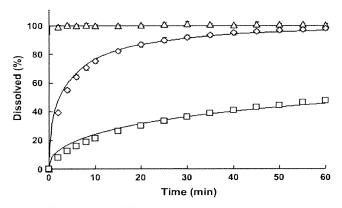


Fig. 2. In vitro dissolution profiles of cilostazol from the suspensions in water at 37 °C. Dissolution study was performed at 50 rpm following USP Apparatus 2. About 5 mg of cilostazol was applied in 900 mL water. Results are expressed as the mean with the bar showing S.D. values of six experiments and simulated curves (solid lines). Keys: Δ, NanoCrystal[®] spray-dried powder; ⋄, jet-milled crystal; □, hammer-milled crystal.

Table 2 Simulated 50% dissolution time ($T_{50\%}$, min) of cilostazol suspensions at 37 °C

Formulation	Dissolution medium				
	Water	FaSSIF	FeSSIF		
NanoCrystal®	0.016	0.016	0.0068		
Jet-milled	2.3	2.3	0.97		
Hammer-milled	82	80	32		

Calculated from simulation results.

3.3.1. Dissolution in water

The dissolution profiles of the cilostazol suspensions in water are shown in Fig. 2. The dissolution rate of cilostazol from the suspensions was clearly affected by the particle size of the active ingredient. From the hammer-milled suspension, only 45% of applied citostazol was dissolved in 60 min. In the case of the jet-milled suspension, more than 80% of cilostazol was dissolved within 15 min and the dissolved fraction reached 95% in 60 min. In contrast, the dissolution of cilostazol from the NanoCrystal[®] suspension was completed immediately. As sub-micron particles such as NanoCrystal® cilostazol can easily pass through a line filter, it is possible to overestimate the dissolution rate. A high-speed centrifugation method [29], therefore, was attempted to separate the solid particles (data not shown), but it was not appropriate because of considerably long time to separate them and the difficulty in controlling temperature during the centrifugation. Although the possible overestimation cannot be excluded, the simulated line agreed with the actual data very well, indicating the extremely rapid dissolution of the NanoCrystal® cilostazol suspension. Visual observation of immediate disappearance of turbidity in the dissolution vessel also suggested that the solid particles passed through the filter could be ignored.

The excellent agreement between the observed data and the simulated dissolution curves suggested that the dissolution of cilostazol from the suspensions followed the Noyes-Whitney equation and that the model with the assumptions and the parameters used were appropriate. The results shown in Fig. 2

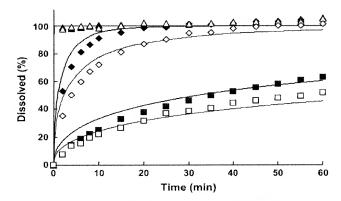


Fig. 3. In vitro dissolution profiles of cilostazol from the suspensions in the biorelevant media at 37 °C. Dissolution study was performed at 50 rpm following USP Apparatus 2. About 5 mg of cilostazol was applied in 900 mL water. Results are expressed as the mean of two experiments and simulated curves (fine lines for FaSSIF and bold lines for FeSSIF). Keys: In FaSSIF: △, NanoCrystal spraydried powder; ⋄, jet-milled crystal; □, hammer-milled crystal; In FeSSIF: △, NanoCrystal spraydried powder; ⋄, jet-milled crystal; □, hammer-milled crystal.

^b For the hammer-milled and the jet-milled suspension.

^c For the NanoCrystal[®] suspension.

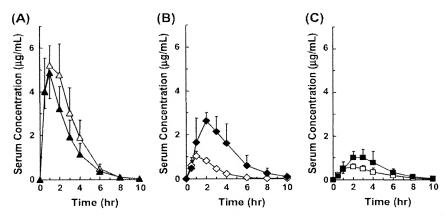


Fig. 4. Serum concentration—time profiles of cilostazol after oral administration of the suspensions at a dose of 100 mg/body in beagle dogs. Results are expressed as the mean with the bar showing S.D. values of four experiments. Keys: (A) Δ, NanoCrystal[®] suspension (fasted); ♠, pet-milled suspension (fed); (B) ♥, jet-milled suspension (fed); (C) □, hammer-milled suspension (fasted); ■, hammer-milled suspension (fed).

were much better than those obtained when cilostazol was treated as monodispersed particles with a mean particle size (data not shown).

Assuming smooth spherical particles, specific surface area is inversely proportional to particle size. Accordingly, the specific surface area of the jet-milled cilostazol crystal and the cilostazol crystal in the NanoCrystal spray-dried powder were calculated as 3.2- and 28-fold greater than that of the hammer-milled crystal, treated as spherical polydispersed particles having size distribution shown in Fig. 1. Based on the simulated curves, 50% dissolution times ($T_{50\%}$) of the hammer-milled, the jet-milled and the NanoCrystal suspensions were calculated to be 82 min, 2.3 min and 0.016 min, respectively (Table 2), indicating that the dissolution rates of the jet-milled and the NanoCrystal suspensions would be 36-fold and 5100-fold greater than that of the hammer-milled suspension, respectively.

3.3.2. Dissolution in bio-relevant media

In order to predict the food effect on the absorption of cilostazol from the suspensions, the dissolution was investigated in the bio-relevant media, FaSSIF and FeSSIF (Fig. 3), because food effects on the extent of absorption of BCS Class II drugs

such as danazol and atovaquone were well correlated with the FeSSIF/FaSSIF ratio of the in vitro dissolved amount [20,30-32]. The data obtained from two vessels for each suspension were superimposed, and the simulated lines agreed fairly well with the observed data. The dissolution rates of cilostazol in FaSSIF were similar to, and those in FeSSIF were faster than those obtained in water for all the suspensions. Simulation study showed that the $T_{50\%}$ values for the hammer-milled, the jetmilled and the NanoCrystal® cilostazol suspensions were 80, 2.3 and 0.016 min in FaSSIF, and 32, 0.97 and 0.0068 min in FeSSIF, respectively (Table 2). Although the FeSSIF/FaSSIF ratio of $T_{50\%}$ for each suspension was around 0.4 regardless of the difference in particle size, the difference in the absolute value of $T_{50\%}$ between FeSSIF and FaSSIF became much smaller as the particle size reduced. Especially, for the NanoCrystal® suspension, it can practically be neglected. These results suggest that the food effect can be avoided by the enhancement of dissolution rate due to the reduction of particle size.

3.4. Bioavailability study in dogs

The serum concentration—time profiles and the pharmacokinetic parameters of cilostazol resulted from the oral admin-

Table 3
Pharmacokinetic parameters

Food condition	Parameter	Intravenous administration (10 mg/kg)	NanoCrystal [®] (100 mg/body)	Jet-milled (100 mg/body)	Hammer-milled (100 mg/body)
Fasted	C _{max} (ng/mL)	NAV.	5371±1173***	1029 ± 218	582±154
Α	AUC (ng h/mL)	17584 ± 7556	17832 ± 4994**	2875 ± 587	2722 ± 803
	t_{max} (h)	name.	1.3 ± 0.5	1.0 ± 0.0	1.8 ± 0.5
	MRT (h)	1.3 ± 0.4	2.4±0.2**	2.3 ± 0.2**	3.6 ± 0.9
	F	1	0.86 ± 0.29	0.15 ± 0.04	0.14 ± 0.05
Fed	C_{max} (ng/mL)	The state of the s	4872±1112***	2901 ± 314**	1152 ± 221
	AUC (ng h/mL)	_	13589±3895**	10669±3417*	4694 ± 1612
	t_{max} (h))-	$1.0 \pm 0.0 *$	1.0 ± 0.0	2.5 ± 1.3
	MRT (h)	8790°	2.3±0.3*	3.4 ± 0.8	3.7 ± 0.6
	F	-	0.67 ± 0.22	0.53 ± 0.21	0.23 ± 0.09

Results are expressed as the mean \pm S.D. of four experiments. ***P<0.001; **P<0.01; *P<0.05, compared to the corresponding parameters of the hammer-milled suspension.

 CL_{total} , k_{cl} and Vd_{ss} for the intravenous administration were calculated to be 5.4 ± 1.8 L/h, 0.79 ± 0.20 h⁻¹ and 6.5 ± 0.7 L, respectively.

Table 4
Fed/fasted ratio on pharmacokinetic parameters

Parameter	NanoCrystal [®] (100 mg/body)	Jet-milled (100 mg/body)	Hammer-milled (100 mg/body)
C_{max}	0.91±0.13	2.9±0.5***	2.0 ± 0.3**
AUC	0.76 ± 0.04	$3.7 \pm 0.7**$	1.8 ± 0.6
$t_{\rm max}$	0.88 ± 0.25	1.8±0.5*	1.0 ± 0.0
MRT	0.95 ± 0.13	1.5 ± 0.4*	1.1 ± 0.4
F	0.78 ± 0.04	3.6 ± 0.7	1.8 ± 0.6

Results are expressed as the mean \pm S.D. of four experiments. ***P<0.001; **P<0.01; *P<0.05, statistically significant difference between the fed state parameters and the fasted state parameters.

istrations of the suspensions in beagle dogs are presented in Fig. 4 and Table 3, respectively. To estimate the food effect, the fed/fasted ratios on the pharmacokinetic parameters were also listed in Table 4.

In the fasted condition, compared with the hammer-milled cilostazol suspension, the absorption of cilostazol was not improved so much by dosing the jet-milled suspension as shown in Fig. 4 and Table 3. On the other hand, the NanoCrystal® suspension significantly increased $C_{\rm max}$ and AUC of cilostazol 9.2 (P < 0.001) and 6.7 times (P < 0.05), respectively, resulting in 86% of the absolute bioavailability. These results indicated that the extensive reduction of particle size could lead to the improvement of bioavailability of cilostazol. Although it was expected that the jet-milled suspension also had improved the bioavailability of cilostazol based on the results of the in vitro dissolution study (Figs. 2 and 3), the absorption was not changed so much, which might be attributed to the difference in dissolution behavior between in vitro and in vivo.

In the fed condition, the $C_{\rm max}$ values of the hammer-milled and the jet-milled suspension were increased 2.0-fold (P < 0.01) and 2.9-fold (P < 0.001), respectively, and the AUC values were increased 1.8-fold (not statistically significant) and 3.7-fold (P < 0.01), respectively (Table 3). These results clearly indicate the positive food effects on the rate and extent of cilostazol absorption for the hammer-milled and the jet-milled suspension. On the other hand, in the case of the

NanoCrystal® suspension, the fed/fasted ratios of $C_{\rm max}$ and the AUC values were 0.91-fold (not statistically significant) and 0.76-fold (not statistically significant), respectively, suggesting slightly negative food effects for the NanoCrystal® suspension.

These results suggest that the in vivo dissolution of cilostazol from the hammer-milled and the jet-milled suspension was improved by the food intake, which could be supported by the absorption rate-time profiles of cilostazol after oral dosing (Fig. 5). As cilostazol is classified into Class II of BCS, the absorption could be rate-limited by the dissolution process. Therefore, the profiles shown in Fig. 5 could reflect the in vivo dissolution behavior as well and clearly indicate that the food intake enhanced and prolonged the dissolution and absorption of cilostazol in the cases of the hammer-milled and the jet-milled suspensions. The prolongation of the dissolution, which is also suggested by the values of MRT (Table 3), might be ascribed to the improvement of dissolution by the food and/ or bile and to the delay of gastric emptying by the food [33]. On the other hand, the dissolution and absorption of cilostazol from the NanoCrystal® suspension were not enhanced and not prolonged by the foods (Table 3 and Fig. 5) because the dissolution might be maximally improved by the size reduction and the drug might partially adsorb to the ingested food. Fig. 5 also shows that initial dissolution/absorption rates in 1 h after administration for the hammer-milled, the jet-milled and the NanoCrystal® cilostazol suspensions were 4.9%, 10.1% and 51.7% in the fasted condition, 4.6%, 14.2% and 50.5% in the fed condition, respectively. These results clearly indicated that the smaller particle resulted in the faster dissolution/absorption. However, it was also shown that food did not enhance the apparent initial absorption rate, which might be explained by the delay of gastric emptying by the food intake [33]. As gastric emptying is another possible rate-limiting step for the absorption, the retardation of gastric emptying could cancel out the potency of the dissolution enhancement.

The particle size reduction certainly enhanced the in vitro dissolution rate and the in vivo dissolution/absorption of cilostazol, but the relationship in the enhancement of dissolution between in vitro and in vivo was not necessarily

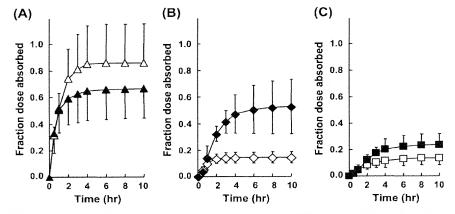


Fig. 5. Absorption rate—time profiles of cilostazol after oral administration of suspensions at a dose of 100 mg/body in beagle dogs. Results are expressed as the mean with the bar showing S.D. values of four experiments. Keys: (A) \triangle , NanoCrystal^{#0} suspension (fasted); \blacktriangle , NanoCrystal^{#0} suspension (fed); (B) \lozenge , jet-milled suspension (fed); (C) \square , hammer-milled suspension (fasted); \blacksquare , hammer-milled suspension (fed).

quantitative. The initial dissolution/absorption rates described above, based on the results shown in Fig. 5, are also obviously larger than the cumulative dissolved amounts for 1 h in the in vitro dissolution study (Fig. 3). It would be difficult to find out the quantitative relationship between in vivo dissolution and in vitro dissolution by a simple dissolution study as employed in the present study, because such a dissolution study is not able to reflect the maintenance and enhancement of the dissolution, which could be ascribed to the sink condition that might be kept to some extent by the sequential absorption right after dissolution in vivo.

In the case of the hammer-milled suspension, which might correspond to the commercial tablet in human study, the bioavailability of cilostazol was enhanced around twice by the food intake, which is in good agreement with the human data where C_{max} and AUC of cilostazol after dosing the commercial 100 mg tablet were 1.7- to 1.9-fold and 1.2- to 1.3-fold greater, respectively, in the fed condition than those in the fasted condition [12]. This food effect would be related with the FeSSIF/FaSSIF ratio in the dissolution rate and/or solubility. This might also be the case with the jet-milled suspension. Although the food effect was a little more significant for the jet-milled cilostazol than that for the hammer-milled one, the enhancement ratios in C_{max} and AUC observed for these suspensions were still comparable to the FeSSIF/FaSSIF ratio in the dissolution rate and/or solubility. On the other hand, the food intake did not increase the bioavailability of the NanoCrystal® cilostazol suspension. Taken all together, the food effect could be independent of the solubility, because the solubility and the FeSSIF/FaSSIF ratio in the solubility were almost same for all the three suspensions. The improvement of dissolution rate should be responsible for the improved bioavailability of cilostazol in the cases of the jet-milled and the hammer-milled suspensions. The reason why no food effect was observed for the NanoCrystal® cilostazol suspension might be that the dissolution rate of NanoCrystal® cilostazol is fast enough even under the fasted condition, where the absorption might be permeability-limited. Therefore, the further increase in the dissolution rate would not contribute to the improvement of the absorption.

4. Conclusion

In the present study, it was demonstrated that the in vitro dissolution rate of cilostazol from aqueous suspension was improved by milling, which was described by the Noyes—Whitney equation. The bioavailability of cilostazol was increased by the reduction of particle size, but remarkable enhancements with minimum food effect were observed for the NanoCrystal® cilostazol suspension, while moderate enhancement of bioavailability and significant food effect were seen in the absorption for the jet-milled suspension, compared to the suspension made of the conventional hammer-milled crystal. These findings clearly indicate that the bioavailability of cilostazol can be maximized and the food effect can be avoided by the NanoCrystal® technology for a robust formulation.

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EXHIBIT 3

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NANOSUSPENSION: AN ATTEMPT TO ENHANCE BIOAVAILABILITY OF POORLY SOLUBLE DRUGS

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ABSTRACT

Most of the new chemical entities coming out from Highthroughput screening in drug discovery process are failing due to their poor solubility in the water. Poorly water-soluble drugs show many problems in formulating them in conventional dosage forms. One of the critical problems associated with poorly soluble drugs is too low bioavailability. The problem is even more complex for drugs belonging to BCS CLASS II category, as they are poorly soluble in both aqueous and organic media, and for those drugs having a log P value of 2. There are number of formulation approaches to resolve the problems of low solubility and low bioavailability. These techniques for solubility enhancement have some limitations and hence have limited utility in solubility enhancement. Nanotechnology can be used to resolve the problems associated with these conventional approaches for solubility and bioavailability enhancement. Nanotechnology is defined as the science and engineering carried out in the nanoscale that is 10-9 meters. The present the details about nanosuspensions. describes article Nanosuspensions consist of the pure poorly water-soluble drug without any matrix material suspended in dispersion. The review article includes the methods of preparation with their advantages and disadvantages, characterization and evaluation parameters and pharmaceutical applications. A nanosuspension not only solves the problems of poor solubility and bioavailability but also alters the pharmacokinetics of drug and thus improves drug safety and efficacy.

INTRODUCTION: Most of the new chemical entities (about 40%) coming out from High-throughput screening in drug discovery process are failing due to their poor solubility in the water ¹. As per a recent report ², 46% of the total New Drug Applications (NDA) filed between 1995 and 2002 were BCS class IV, while only 9% were BCS class I drugs, revealing that a majority of the approved new drugs were water insoluble Because of their poor solubility it will become more complicated to incorporate them into the conventional dosage forms and thus decreasing the bioavailability of the drugs ³.

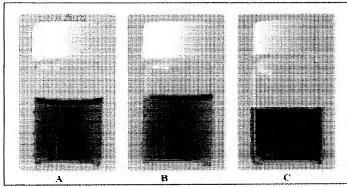
The problem is even more complex for drugs such as Glibenclamide (belonging to BCS CLASS II) as classified by BCS System ⁴ as they are poorly soluble in both aqueous and organic media, and for those drugs having a log P value of 2. For class II drugs, the rate limiting factor in their intestinal absorption is dissolution/solubility and thus the performance of these drugs is dissolution rate-limited and is affected by the fed/fasted state of the patient. Dissolution rates of sparingly soluble drugs are greatly affected by the shape as well as the particle size of the drug. Therefore decrease in particle size results in an increase in dissolution rate 5. There are number of formulation approaches that can be used to resolve the problems associated with the low solubility and low bioavailability of these class II drugs. Some of the approaches to increase solubility include micronization ⁶, solubilisation using cosolvents, use of permeation enhancers, oily solutions, surfactant dispersions ⁶, salt formation ⁷ and precipitation techniques 8-9.

Most of these techniques for solubility enhancement have advantages as well as some limitations and hence have limited utility in solubility enhancement. Other techniques used for solubility enhancement like microspheres, emulsions, microemulsions ¹⁰, liposomes ¹¹, super critical processing, solid-dispersions ¹² and inclusion

complexes using Cyclodextrins ¹³ show reasonable success but they lack in universal applicability to all drugs. These techniques are not applicable to the drugs, which are not soluble in both aqueous and organic Media.

However, there still remains an unmet need to equip the pharmaceutical industry with particle engineering technologies capable of formulating the poorly soluble drugs to improve their efficacy and therapy with respect optimize pharmacoeconomics. One such novel technology is nanosuspension technology. Nanosuspensions are sub-micron colloidal dispersions of nanosized drug surfactants particles stabilized bv Nanosuspensions consist of the poorly watersoluble drug without any matrix material suspended in dispersion 15. These can be used to enhance the solubility of drugs that are poorly soluble in aqueous as well as lipid media. As a result of increased solubility, the rate of flooding of the active compound increases and the maximum plasma level is reached faster.

This is one of the unique advantages that it has over other approaches for enhancing solubility. This approach is useful for molecules with poor solubility, poor permeability or both, which poses a significant challenge for the formulators. The reduced particle size renders the possibility of intravenous administration of poorly soluble drugs without any blockade of the blood capillaries. The suspensions can also be lyophilised and into a solid matrix. Apart from these advantages it is also having the advantages of liquid formulations over others. In the present review we are mainly focussing on the different methods of preparation, critical parameters and evaluation nanosuspension. Fig. 1 shows some of the nanosuspensions 16.



A- Gold nanosuspension in water, **B**-Silver nanosuspension in water, **C**-VOPc (vanadyl phthalocyanine) nanosuspension in water

FIGURE 1: FEW TYPES OF NANOSUSPENSIONS.

Nanosuspensions differ from nanoparticles ¹⁷ which are polymeric colloidal carriers of drugs (Nanospheres and nanocapsules), and from solid-lipid nanoparticles ¹⁸ (SLN), which are lipidic carriers of drug. The potential benefits of nanoparticles over conventional technologies are described in **Table 1**

TABLE 1: POTENTIAL BENEFITS OF NANOSUSPENSION TECHNOLOGY

ROUTE OF ADMINISTRATION	POTENTIAL BENEFITS
Oral	 Rapid dissolution and High bloavailability Reduced fed/fasted ratio
Intravenous (I.V)	 Tissue targeting RapId dissolution Longer duration of retention in systemic circulation
Ocular	Higher bioavallabilityLess irritationMore consistent dosing
Inhalation	Higher bioavallabilityMore consistent dosing
Subcutaneous/ intramuscular	Higher bioavailabilityRapid onsetReduced tissue irritation

Preparation of Nanosuspensions: Preparation of nanosuspensions were reported to be a more cost effective and technically more simpler alternative than liposomes and other conventional colloidal drug carriers, particularly for poorly soluble drugs and yield a physically more stable product. The simplest method of preparation of nanosuspensions is micronization by colloid or jet milling 20, which improves the dissolution rate but is not having any effect on saturation solubility. Nanosuspension processes currently used are engineering preparation by precipitation, high pressure homogenization, emulsion and milling techniques. These techniques and the obtained compounds are summarized in Table 2 and are briefly described in the following sections. Mainly there are two methods for preparation of nanosuspensions. The conventional methods of precipitation are called technology'. The Top Down 'Bottom Up Technologies' are the disintegration methods and are preferred over the precipitation methods. These include Media Milling (Nanocrystals), High Pressure Homogenization in water (Dissocubes), High Pressure Homogenization in nonaqueous media (Nanopure) and combination of Precipitation and High-Pressure Homogenization (Nanoedege). Few techniques used preparing other emulsion as templates, nanosuspensions are microemulsion as templates etc.

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• Precipitation: The most common method of precipitation used is anti solvent addition method in which the drug is dissolved in an organic solvent and this solution is mixed with a miscible antisolvent. Mixing processes vary considerably. Precipitation has also been coupled with high shear processing. The NANOEDGE process (is a registered trademark of Baxter International Inc. and its subsidiaries) relies on the precipitation of friable materials for subsequent fragmentation under conditions of high shear and/or thermal energy ³².

TABLE 2: SUMMARY OF THE NANOSUSPENSION FORMATION TECHNOLOGIES

Technology	Advantage	Disadvantage	Drug
Precipitation	Simple process. Ease of scale up. Economical production.	Growing of crystals needs to be limit by surfactant addition. Drug must be soluble at least in one solvent.	Carbamazepine ⁸ Cyclosporine ²¹ Griseofulvin ²²
Ernulsion/Microemulsion template	High drug solubilization. Long shelf life. Ease of manufacture.	Use of high amount of surfactant and stabilizers. Use of hazardous solvent in production.	Breviscapine ²³ Griseofulvin ²⁴
High pressure Homogenization	Applicable to most of the drugs Very dilute as well as highly concentrate nanosuspension can be prepared. Aseptic production possible.	High number of homogenization cycles. Drug should be in micronized state. Possible contamination could occur from metal ions coming off from the	Albendazole ²⁵ Aphidicolin ²⁶ Azithromycin ²⁷ Fenofibrate ²⁸
Milling methods • Media milling	Applicable to the drugs that are poorly soluble in both aqueous and organic media. Little batch to batch variation. High flexibility in handling large quantities of drugs.	walls. Time consuming. Difficult to scale up. Prolonged milling may induce the formation of amorphous & instability.	Cilostazol ²⁹ Danazol ³ Naproxen ³
 Dry Co-grinding 	Easy process and no organic solvent required. Require short grinding time.	Generation of residue of milling media.	Clarithromycin ³⁰ Glibenclamide ³¹

This is accomplished by a combination of rapid precipitation and high-pressure homogenization. Rapid addition of a drug solution to an antisolvent leads to sudden super saturation of the mixed solution, and generation of fine crystalline or amorphous solids. Precipitation of an amorphous material may be favored at high super saturation when the solubility of the amorphous state is exceeded. The success of drug nanosuspensions prepared by precipitation techniques has been reported in some journals ³²⁻³³.

 Lipid Emulsion/Microemulsion Template: Lipid emulsions as templates are applicable for drugs that are soluble in either volatile organic solvents or partially water miscible solvents. In this method the drug will be dissolved in the suitable organic solvent and then emulsified in aqueous phase using suitable surfactants. Then the organic solvent will be slowly evaporated under reduced pressure to form drug particles precipitating in the aqueous phase forming the aqueous suspension of the drug in the required particle size. Then the suspension formed can be suitably to get nanosuspensions diluted as templates microemulsions Moreover, produce nanosuspensions. Microemulsions thermodynamically stable and isotropically clear dispersions of two immiscible liquids such as oil and

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water stabilized by an interfacial film of surfactant and co-surfactant. The drug can be either loaded into the internal phase or the pre-formed microemulsion can be saturated with the drug by Suitable dilution intimate mixing. microemulsion yields the drug nanosuspension 34. An example of this technique is the griseofulvin is prepared nanosuspension which microemulsion 34. The advantages of lipid emulsions as templates for nanosuspension formation are that they easy to produce by controlling the emulsion droplet and easy for scale-up. However, the use of organic solvents affects the environment and large amounts of surfactant or stabilizer are required.

used method for the preparation of the nanosuspensions of many poorly water soluble drugs 35-37. Different methods developed based on this principle for preparation of nanosuspensions are Dissocubes, Nanopure, Nanoedge, Nanojet technology. In the high pressure homogenization method, the suspension of a drug and surfactant is forced under pressure through a nanosized aperture valve of a high pressure homogenizer.

The principle of this method is based on cavitation in the aqueous phase. The particles cavitations forces are sufficiently high to convert the drug microparticles into nanoparticles. The concern with this method is the need for small sample particles before loading and the fact that many cycles of homogenization are required ³⁸⁻³⁹. Figure 2 gives the schematic representation of the high-pressure homogenization process

DissoCubes technology is an example of this technology developed by R.H. Müller using a piston-gap-type high pressure homogenizer, which was recently released as a patent owned by SkyePharm plc ³⁴. Scholer et al. prepared atovaquone nanosuspensions using this technique.

 Nanopure is suspensions homogenized in water-free media or water mixtures.

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- Nanoedge is combination of precipitation and homogenization techniques resulting in smaller particle size and better stability in a shorter time.
- Nanojet technology, also called as opposite stream, uses a chamber where a stream of suspension is divided into two or more parts, which colloid with each other at high pressure.

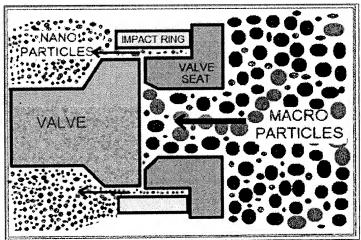


FIGURE 2: SCHEMATIC CARTOON OF THE HIGH-PRESSURE HOMOGENIZATION PROCESS

• Milling Techniques:

Media milling: Media milling is a further technique used to prepare nanosuspensions ²⁴, ⁴⁰. This patent-protected technology was developed by Liversidge et al. ⁴¹. Formerly, the technology was owned by the company NanoSystems but recently it has been acquired by Elan Drug Delivery. In this technique, the nanosuspensions are produced using high-shear media mills or pearl mills. The media mill consists of a milling chamber, a milling shaft and a recirculation chamber. The drug nanoparticles are obtained by subjecting the drug to media milling. High energy and shear

forces generated as a result of impaction of the milling media with the drug provide the necessary energy input to disintegrate the microparticulate drug into nanosized particles. The milling medium is usually composed of glass, zirconium oxide or highly cross-linked polystyrene resin. In batch mode, the time required to obtain dispersions with unimodal distribution profiles and mean diameters <200nm is 30–60 min. In the media milling process, the milling chamber is charged with the milling media, water or suitable buffer, drug and stabilizer. Then milling media or pearls are rotated at a very high shear rate.

Dry Co-Grinding: Recently, nanosuspensions can be obtained by dry milling techniques. preparing work in stable Successful nanosuspensions using dry-grinding of poorly soluble drugs with soluble polymers and copolymers after dispersing in a liquid media has been reported 42. Itoh et al 35 reported the colloidal particles formation of many poorly water soluble drugs; griseofulvin, glibenclamide and nifedipine obtained by grinding with (PVP) and sodium polyvinylpyrrolidone dodecylsulfate (SDS).

Many soluble polymers and co-polymers such as PVP, polyethylene glycol (PEG), hydroxypropyl methylcellulose (HPMC) and cyclodextrin derivatives have been used ⁴³. Physicochemical properties and dissolution of poorly water soluble drugs were improved by co-grinding because of an improvement in the surface polarity and transformation from a crystalline to an amorphous drug ⁴⁴. Dry cogrinding can be carried out easily and economically and can be conducted without organic solvents. The co-grinding technique can reduce particles to the submicron level and a stable. Table 3 shows some drugs and their status in market.

TABLE 3: SOME DRUGS AND THEIR STATUS IN MARKET

Drug	Category	Route of Administration	Status
Fenofibrate	Anticancer	Oral	Phase I
Rapamuane	Antiemetic	Oral	Marketed
Emend	Antiasthamatic	Oral	Market ed
Thymectacin	Antidiabetic	1.V.	Phase I/II
Silver	Eczema, Atopic dermatitis	Topical	Phase I
Busulfan	Hypolidemic	Intrathecal	Phase I
Paclitaxel	Anticancer	I. V.	Phase IV
Insulin	Antidiabetic	Oral	Phase I
Budesonide	Anticancer	Pulmonary	Phase I

Physical, Chemical and Biological Properties of Nanosuspensions: Nanosuspension formulation increases the saturation solubility as well as dissolution rate. Basically the saturation solubility is a compound specific constant which is temperature dependent. The saturation solubility also depends on the polymorphism of the drug as different polymorphs have different solubilities. It is also dependent on the particle size. This size-depend encycomes only into effect for particles having a size below approximately 1 μm. Another marked property is the adhesiveness generally described for nanoparticles ⁴⁵.

As the particle size decreases the adhesive properties of the particles will be improved and thus improved oral delivery of poorly soluble drugs. dose bioavailability, improved **Improved** reduced fed/fasted variability, proportionality, reduced inter-subject variability and enhanced absorption rate (both human and animal data) 46 are some of the main effects observed on oral administration. These data have been acquired in vivo in animals but also in humans as reported by the company Nano Systems. A drastically remarkable report is that of the increase in bioavailability for danazole from 5 % (as macrosuspension) to 82% (as nanosuspension) 46. The application of high pressures during the production of nanosuspensions was found to promote the amorphous state ⁴⁷. The degree of particle fineness and the fraction of amorphous particles in the nanosuspensions were found to be dependent on production pressure number of cycles of homogenisation and hardness of drug. The increase in the amorphous fraction leads to a further increase of the saturation solubility. The homogenization process (giving uniform particle size) was able to overcome Ostwald ripening ⁴⁸ which means physical long-term stability as an aqueous suspension ⁴⁹.

ln drug administration, the oral bioavailability mainly depends upon the solubility of the drug, highly active compounds have failed in the past because their poor solubility has limited in vivo absorption and did not lead to effective therapeutic concentrations. As an example, Atovaquone is given orally three times 750 mg daily, because of the low absorption of only 10-15%. Oral administration of nanosuspensions can overcome this problem because of the high adhesiveness of drug particles sticking on biological surfaces and prolonging the absorption time.

Evaluation of Nanosuspensions ⁵⁰⁻⁵¹: The characterisation of the nanosuspensions is also similar to that of the suspensions such as colour, odour, presence of impurities and other important characteristics as mentioned below.

- In-Vitro Evaluations:
 - Particle size and size distribution
 - Particle charge (Zeta Potential)
 - Crystalline state and morphology
 - Saturation solubility and dissolution velocity
 - Stability
- In-vivo evaluation:
- In-Vitro Evaluations:

Particle size and size distribution: It is the most important parameter in the evaluation of the suspensions as it is having the direct effect on the solubility and dissolution rate and the physical stability of the formulation. The mean particle size and the width of particle size can Photon Correlation determined bν Spectroscopy (PCS) 52, laser diffraction and coulter current multisizer. Particle size and polydispersity index (PI) governs the saturation solubility, dissolution velocity and biological performance. PCS measures the particle size in the range of 3nm-3 µm only. PI governs the physical stability of nanosuspension and should be as low as possible for long-term stability (Should be close to zero). LD measures volume size distribution and measures particles ranging from 0.05-80µm upto 2000µm. Atomic Force Microscopy is used for visualization of particle shape 53. For IV use, particles should be less than 5 µm, considering that the smallest size of the capillaries is 5-6 µm and hence a higher particle size can lead to capillary blockade and embolism.

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- Particle charge (Zeta Potential): The particle charge is of importance in the study of the stability of the suspensions. Usually the zeta potential of more than ±40mV will be considered to be required for the stabilisation of the dispersions. For electrostatically stabilized nanosuspension a minimum zeta potential of ±30mV is required and in case of combined steric and electrostatic stabilization it should be a minimum of ±20mV of zeta potential is required.
- Crystalline Sate and Particle Morphology: It is
 of importance as there are chances of the
 polymorphism during the storage of the
 nanosuspensions. Hence it is necessary to study
 the crystal morphology of the drug in
 suspension. Differential Scanning Calorimetry

(DSC) is most commonly used for such studies ⁵⁴. When nanosuspensions are prepared drug particles may get converted to amorphous form hence it is essential to measure the extent of amorphous drug generated during the production of nanosuspensions. The X-Ray Diffraction (XRD) is commonly used for determining change in crystallinity and the extent of the amorphous form of drug ⁵⁵.

- Saturation solubility and Dissolution Velocity: The main advantage associated with the nanosuspensions is improved saturation solubility as well as dissolution velocity. These are studied in different physiological solutions at different pH. Kelvin equation and the Ostwald-Freundlich equations can explain increase in saturation solubility. Determination of these parameters is useful to assess in vivo performance of the formulation.
- Stability of Nanosuspensions: Stability of the suspensions is dependent on the particle size. As the particle size reduces to the nanosize the surface energy of the particles will be increased and they tend to agglomerate. So stabilizers are used which will decrease the chances of Ostwald ripening and improving the stability of the suspension by providing a steric or ionic barrier. Typical examples of stabilizers used in nanosuspensions are cellulosics, poloxamer, polyoleate and lecithin, polysorbates, povidones. Lecithin may be preferred in developing parenteral nanosuspensions 40.
- In vivo evaluation: The in vivo evaluation of the nanosuspensions is specific to drug and route of administration. Most commonly the formulation was given by required route of administration and the plasma drug levels were estimated using HPLC-UV visible Spectrophotometry. Other parameters which are generally evaluated in vivo are

- Surface hydrophilicity/hydrophobicity (determines interaction with cells prior to phagocytosis)
- Adhesion properties
- · Interaction with body proteins

drug **APPLICATIONS: Formulating** the as increases the saturable nanosuspensions well concentration, dissolution rate as bioavailability of the drug. These nanosuspensions are having application in different routes of parenteral, topical, administrations like oral, ophthalmic, mucoadhesive, pulmonary and targeted Oral administration drug delivery. nanosuspensions is a drug delivery strategy, not only to improve bioavailability, but also to target gastrointestinal bacterial and parasitic infections adhesion properties. because of improved Nanosuspension technology is considered as suitable new colon delivery systems for the treatment of colon cancer, helminth infections, gastrointestinal inflammation or GIT associated diseases like sprue (zoeliaki).

Infections like tuberculosis, listeriosis, leishmaniasis, and toxoplasmosis are caused by parasites residing the macrophages of the MPS, thus being relatively easily accessible by I.V. injected particles. The I.V. injected particles are heavily and quickly taken up by the MPS cells in case they absorb uptake promoting proteins like apolipoproteins. However, some parasites do also reside in the brain (CNS). The brain-localized parasite mostly leads to relapsing infections if not cured. Therefore, it would be of importance to target drug nanoparticles via surface modification to the brain. A successful targeting of the peptide, dalargin, to the brain using Tween 80® surface modified polyisobutylcyanoacrylates nanoparticles has been reported by Kreuter et al. 56. A nanosuspension of Amphotericin B developed by Kayser et al. showed a significant improvement in its oral absorption in comparison with the conventional commercial formulations 57 . In case of I.V administration the particle size less than 5µm is preferred. The particle size in nano range will favour the passage of the drug particles into the small capillaries in the body without any blockade. A stable intravenously injectable formulation of omeprazole has been prepared to prevent the degradation of orally administered omeprazole 37 .

Aqueous suspensions of the drug can be easily nebulised and given by pulmonary route as the particle size is very less. Different types of nebulisers are available for the administration of liquid formulations. Some of the drugs successfully tried with pulmonary route are budesonide, ketotifen, ibuprofen, indomethacin, nifedipine, itraconazole, interleukin-2, p53 gene, leuprolide, doxorubicin etc. 58 Nanosuspensions can be used for targeted delivery also as the surface of the particle can be suitably modified to make them target specific. Kayser formulated a nanosuspension of Aphidicolin to improve drug targeting against leishmania-infected macrophages ²⁶. Scholer et al. Prapeared a nanosuspension formulation Atovaquone and showed an improved drug targeting to the brain in the treatment of toxoplasmic encephalitis in a new murine model infected with Toxoplasma gondii 55.

conclusions: Nanosuspensions are chiefly seen as vehicles for administering poorly water soluble drugs have been largely solved the dissolution problems to improve drug absorption and bioavailability. Nanosuspension technology can be combined with traditional dosage forms: tablets, capsules, pellets, and can be used for parenteral products. They have recently received increasing attention as colloidal carriers for targeted delivery of various anticancer drugs, photosensitizers, neutron capture therapy agents or diagnostic agents. Because of their submicron size they are easily targeted to the tumour area. Moreover the possibility of surface functionalization with a

targeting moiety has open new avenues for targeted delivery of drugs, genes, photosensitizers and other molecules to the desired area. To take advantage of nanosuspension drug delivery, simple formation technologies and variety applications, nanosuspensions will continue to be of interest as oral formulations and non-oral administration develop in the future. It is expected that future research and development work will be carried out in the near future for clinical realization of these targeted delivery vehicle.

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EXHIBIT 4



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Physical and chemical stability of drug nanoparticles

ABSTRACT

discussed.

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1. Introduction

As nano-sizing is becoming a more common approach for pharmaceutical product development, researchers 19

are taking advantage of the unique inherent properties of nanoparticles for a wide variety of applications. This 20

article reviews the physical and chemical stability of drug nanoparticles, including their mechanisms and 21

corresponding characterization techniques. A few common strategies to overcome stability issues are also 22

With significant attention focused on nanoscience and nanotech- 54 nology in recent years, nanomaterial-based drug delivery has been 55 propelled to the forefront by researchers from both academia and 56 industry [1-3]. Various nano-structured materials were produced and 57 applied to drug delivery such as nanoparticles [4], nanocapsules [5], 58

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nanotubes [6], micelles [7], microemulsions [8] and liposomes [9]. In general, the term "nanoparticles" refers to particles with sizes between 1 and 100 nm. However, submicron particles are also commonly referred as nanoparticles in the field of pharmaceutics and medicine [10-14]. Nanoparticles are categorized as nanocrystals [10], polymeric [15], liposomal [9] and solid lipid nanoparticles (SLN) [16] depending on their composition, function and morphology. Given the extensive available literature reviews on SLN, polymeric and liposomal nanoparticles [4,9,15-18], this article will focus only on nanocrystals (pure drug nanoparticles).

The unique nano-scale structure of nanoparticles provides significant increases in surface area to volume ratio which results in notably different behavior, both in-vitro and in-vivo, as compared to the traditional microparticles [10-12]. Consequently, drug nanocrystals have been extensively used in a variety of dosage forms for different purposes [10,11,14,19,20], such as improving the oral bioavailability of poorly water-soluble drugs by utilizing enhanced solubility and dissolution rate of nanoparticles [21-23]. In the field of pulmonary drug delivery, the nanoparticles are able to deliver the drugs into the deep lungs, which is of great importance for systemically absorbed drugs [11,14]. In addition, injection of poorly water-soluble nanosuspension drugs is an emerging and rapidly growing field that has drawn increasing attention due to its benefits in reducing toxicity and increasing drug efficacy through elimination of co-solvent in the formulation [10,20].

Despite the advantages of drug nanocrystals, they present various drawbacks including complex manufacturing [12.24-26], nanotoxicity [27] and stability issues [10,19,20]. Stability is one of the critical aspects in ensuring safety and efficacy of drug products. In intravenously administered nanosuspensions, for example, formation of larger particles (>5 µm) could lead to capillary blockade and embolism [20], and thus drug particle size and size distribution needs to be closely monitored during storage. The stability issues of drug nanoparticles could arise during manufacturing, storage and shipping. For instance, the high pressure or temperature produced during manufacturing can cause crystallinity change to the drug particles [12,26,28]. Storage and shipping of the drug products may also bring about a variety of stability problems such as sedimentation, agglomeration and crystal growth [29-31]. Therefore, stability issues associated with drug nanocrystals deserve significant attention during pharmaceutical product development. This article reviews existing literature on drug nanoparticle stability, including theory/mechanisms, methods used to tackle the stability problems and characterization techniques, and provides recommendations to improve the current practices. Since the stability issues related to nanoparticle dry powders are usually trivial, this review will only focus on stability of nanosuspensions (drug nanoparticles dispersed in a liquid medium).

2. Stability of drug nanoparticles

2.1. Effect of dosage form on stability

The unique characteristics of drug nanoparticles have enabled their extensive application in various dosage forms including oral, parenteral, ocular, pulmonary, dermal and other specialized delivery systems [10,11,13,20,32]. Although different dosage forms may share some common stability issues, such as sedimentation, particle agglomeration or crystal growth, their effects on drug products are quite different. For instance, particle agglomeration could be a major issue in pulmonary drug delivery since it affects deposition amount/ site, and thus drug efficacy. On the other hand, agglomeration in intravenous formulations can cause blood capillary blockage and obstruct blood flow. Moreover, the selection of stabilizers is also closely related to dispersion medium, dosage form and strictly governed by FDA regulations. To date, there is a wide variety of choices on the approved stabilizers for oral dosage form whereas the 121 excipients allowed for inhalation are very limited [33].

Drug nanoparticles exist in the final drug products either in dry 123 powder or suspension form. Examples of the dry powder form include 124 the dry powder inhaler, lyophililized powder for injection and oral 125 tablets or capsules. Solid dosage forms usually have good storage 126 stability profiles, which is why a common strategy to enhance 127 nanosuspension stability is to transform the suspension into solid 128 form [19,25]. Most of the reported stability concerns arise from 129 nanosuspensions in which the drug nanoparticles are dispersed in a 130 medium with or without stabilizers. In addition, mechanisms 131 involved in the stability of small and large biomolecule formulations 132 are different due to their molecular structure differences. A small 133 molecule drug is defined as a low molecular weight non-polymeric 134 organic compound while large biomolecules refer to large bioactive 135 molecules such as protein/peptide. One of the major issues with 136 protein/peptide stability is to maintain the 3-dimensional molecular 137 conformation, such as secondary and tertiary structure in order to 138 keep their biological activities [34,35], whereas there is no such 139 concern for small organic molecules.

2.2. General stability issues related to nanosuspensions

Stability issues associated with nanosuspensions have been widely 142 investigated and can be categorized as physical and chemical stability. 143 The common physical stability issues include sedimentation/cream- 144 ing, agglomeration, crystal growth and change of crystallinity state.

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2.2.1. Sedimentation or creaming

Drug particles can either settle down or cream up in the 147 formulation medium depending on their density relative to the 148 medium. The sedimentation rate is described by Stokes' law [36,37] 1-19 which indicates the important role of particle size, medium viscosity 150 and density difference between medium and dispersed phase in 151 determining the sedimentation rate. Decreasing particle size is the 152 most common strategy used to reduce particle settling. Matching drug 153 particles density with medium or increasing medium viscosity are the 154 other widely used approaches to alleviate sedimentation problems 155 [37,38]. Fig. 1 shows different sedimentation types that occur in 156 suspension formulations.

In a deflocculated suspension (Fig. 1a), particles settle indepen- 158 dently as small size entities resulting in a slow sedimentation rate. 159 However, densely packed sediment, known as caking [39], is usually 160 formed due to the pressure applied on each individual particle. This 161 sediment is very difficult to be re-dispersed by agitation [36,37,39] 162 and would be detrimental to the drug products performance. In the 163 flocculated suspension (Fig. 1b), the agglomerated particles settle as 164 loose aggregates instead of as individual particles [36,37]. The loose 165 aggregates have a larger size compared to the single particle, and thus 166higher sedimentation rate. The loose structure of the rapidly settling 167 flocs contains a significant amount of entrapped medium and this 168 structure is preserved in the sediment. The final flocculation volume is 169 therefore relatively large and the flocs can be easily broken and re- 170 dispersed by simple agitation. K.P. Johnston et al. [40,41] have 171 recently attempted to achieve stable nanosuspensions via a novel 172 design of flocs structure called "open flocs", as illustrated in Fig. 1c. 173 Thin film freezing was used to produce BSA nanorods with aspect 174 ratio of approximately 24. These BSA nanorods were found to be 175 highly stable when dispersed into hydrofluoroalkane (HFA) propel- 176 lant, with no apparent sedimentation observed for 1 year. Due to the 177 high aspect ratio of BSA nanorods and relatively strong attractive Van 178 der Waals (VDW) forces at the contact sites between the particles, 179 primary nanorods were locked together rapidly as an open structure 180 upon addition of HFA, inhibiting collapse of the flocs [41]. The low- 181 density open flocs structure was then filled with liquid HFA medium, 182 preventing particle settling. Similar results were shown using needle 183

Fig. 1. Sedimentation in (a) deflocculated suspension; (b) flocculated suspension; and (c) open flocs-based suspension.

and plate shaped itraconazole nanoparticles with aspect ratios between 5 and 10 [40].

Although sedimentation is one of the key issues for colloidal suspension, the reported studies examining sedimentation issues in aqueous-based nanosuspensions are very scarce. This could be due to (i) surfactants are generally used in most of the nanosuspensions to inhibit particle agglomeration in the medium, which alleviates the sedimentation issues and (ii) the small nano-sized particles significantly reduce the sedimentation rate. In addition, many of the aqueous nanosuspensions are transformed to dry solid form by spray drying or freeze drying to circumvent the long-term sedimentation issue. Unfortunately, this solidification process cannot be applied to non-aqueous nanosuspensions where sedimentation/creaming is commonly present. An example to illustrate this is metered dose inhaler (MDI) formulations where the nanoparticles are suspended in HFA propellants. Sedimentation or creaming is a key aspect affecting stability of these formulations. Particle engineering to optimize particle surface properties and morphology, e.g. hollow porous particles [42], and introduction of surfactant(s) is generally employed to alleviate the issue.

2.2.2. Agglomeration

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The large surface area of nanoparticles creates high total surface energy, which is thermodynamically unfavorable. Accordingly, the particles tend to agglomerate to minimize the surface energy. Agglomeration can cause a variety of issues for nanosuspensions including rapid settling/creaming, crystal growth and inconsistent dosing. The most common strategy to tackle this issue is to introduce stabilizers to the formulation. In addition to safety and regulation

considerations, selection of stabilizers is based on their ability to 212 provide wetting to surface of the particles and offer a barrier to 213 prevent nanoparticles from agglomeration [13,19].

There are two main mechanisms through which colloidal suspen- 215 sions can be stabilized in both aqueous and non-aqueous medium, i.e. 216 electrostatic repulsion and steric stabilization [10,36,37]. These two 217 mechanisms can be achieved by adding ionic and non-ionic stabilizers 218 into the medium, respectively. Stabilization from electrostatic 219 repulsion can be described by the classic Derjaguin-Landau- 220 Verwey-Overbeek (DLVO) theory [43,44]. This theory mainly applies 221 to aqueous suspension while its application in non-aqueous medium 222 is still not well-understood [33]. The DLVO theory assumes that the 223 forces acting on the colloidal particles in a medium include repulsive 224 electrostatic forces and attractive VDW forces. The repulsive forces are 225 originated from the overlapping of electrical double layer (EDL) 226 surrounding the particles in the medium, and thus preventing 227 colloidal agglomeration. The EDL consist of two layers: (i) stern 228 layer composed of counter ion attracted toward the particle surface to 229 maintain electrical neutrality of the system and (ii) Gouy layer which 230 is essentially a diffusion layer of ions (Fig. 2).

The total potential energy (V_T) of particle-particle interaction is a 232 sum of repulsion potential (V_R) generated from electric double layers 233 and attraction potential (V_R) from the VDW forces. V_A is determined 234 by the Hamaker constant, particle size and inter-particulate distance 235 while V_R depends on particle size, distance between the particles, zeta 236 potential, ion concentration and dielectric constant of the medium. V_R 237 is extremely sensitive to ion concentration in the medium. As the ion 238 strength is increased in the medium, the thickness of EDL decreases 239 due to screening of the surface charge [36,37]. This causes decrease in 240 V_R , increasing the susceptibility of the dispersed particles to form 241 aggregates. Zeta potential (ZP) is electric potential at the shear plane 242 which is the boundary of the surrounding liquid layer attached to the 243 moving particles in the medium. ZP is a key parameter widely used to 244 predict suspension stability. The higher the ZP, the more stable the 245 suspension is.

In the case of steric stabilization, amphiphilic non-ionic stabilizers 247 are usually utilized to provide steric stabilization which is dominated 248 by solvation effect. As the non-ionic stabilizers are introduced into 249 nanosuspensions, they are absorbed onto the drug particles through 250 an anchor segment that strongly interacts with the dispersed 251 particles, while the other well-solvated tail segment extends into 252 the bulk medium (Fig. 3).

As two colloidal particles approach each other, the stabilizing 254 segments may interpenetrate, squeezing the bulk medium molecules 255 out of the inter-particulate space as illustrated in Fig. 3. This 256 interpenetration is thermodynamically disfavored when a good 257 solvent is used as the bulk medium to stabilize the tail [36], 258 Accordingly, provided that the stabilizers can be absorbed onto the 259 particle surface through the anchor segment, strong enthalpic 260 interaction (good solvation) between the solvent and the stabilizing 261 segment of the stabilizer is the key factor to achieve steric 262 stabilization and prevent particles from agglomeration in the medium 263 [36,37]. In addition to solvation, the stabilizing moiety needs to be 264 sufficiently long and dense to maintain a steric barrier that is capable 265 of minimizing particle-particle interaction to a level that the VDW 266 attractive forces are less than the repulsive steric forces [43–45].

The main drawback associated with the steric stabilization is the 268 constant need to tailor the anchoring tail according to the particular 269 drug of interest. Due to the lack of fundamental understanding of 270 interaction between the stabilizers and dispersed nanoparticles, 271 current surfactant screening approaches to achieve a successful steric 272 stabilization are mostly empirical and could be very burdensome [45–273 49]. In addition, the solvation of the stabilizing segment is susceptible 274 to variation in temperature. Stabilizer concentration could also play a 275 role in causing suspension instability by affecting the absorption 276 affinity of non-ionic stabilizers to drug particles surface. Deng et al. 277

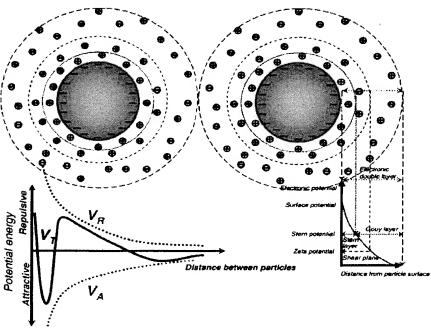


Fig. 2. Illustration of classical DLVO theory. Attractive forces are dominant at very small and large distances, leading to primary and secondary minimum, while repulsive forces are prevailing at intermediate distances and create net repulsion between the dispersed particles, thus preventing particle agglomeration.

[50] used Pluronic® F127 to stabilize paclitaxel nanosuspensions. It was reported that stabilizers had high affinity to nanocrystals surface at concentrations below critical micelle concentration (CMC), and increasing concentrations above CMC caused loss of F127 affinity to the nanocrystals and thus unstable formulation. This was because F127 monomers on the nanocrystals surface started to aggregate with each other to form micelles as the concentration was increased to the CMC level, leading to a lower affinity to the drug crystals. Temperature was also shown to affect the stabilizer affinity to drug crystals. This is expected since the CMC level is dependent on temperature.

It is apparent that combination of the two stabilization mechanisms can be very beneficial in achieving a stable colloidal dispersion. In addition, the combination of a non-ionic stabilizer with an ionic stabilizer reduces the self repulsion between the ionic surfactant molecules, leading to closer packing of the stabilizer molecules [10,51].

Besides the steric and electrostatic stabilization mechanisms, some 293 other stabilization mechanisms have also been reported. Makhlof et 294 al. produced indomethacin (IMC) nanocrystals using the emulsion 295 solvent diffusion technique [52]. The nanoparticles were stabilized 296 using various cyclodextrins (CyDs) without adding any surfactants. 297 The stabilizing effect was attributed to the formation of a CyD network 298 in the aqueous medium via intermolecular interaction of CyD 299 molecules. The network-like structure was believed to prevent 300 aggregation and crystal growth of IMC nanoparticles initially 301 produced from the solvent diffusion process. Similar stabilization 302 mechanism was also observed in another study where budesonide 303 microsuspension was stabilized with hydroxypropyl-beta-cyclodex-304 trin in HFA medium [53]. Another approach to enhance suspension 305 stability that has increasingly been utilized is engineering of particle 306 morphology. One breakthrough in this area was the porous particle 307

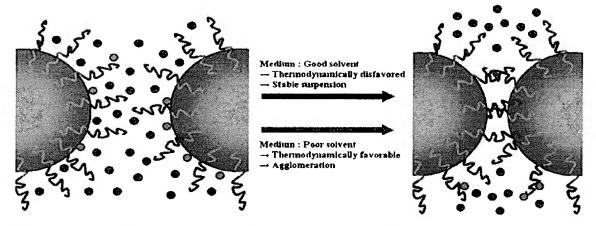


Fig. 3. Steric stabilization mechanisms according to Gibbs free energy: ΔG = ΔH-TΔS. A positive ΔG indicates stable suspension while negative ΔG induces particle agglomeration. If the medium is a good solvent for the stabilizing moiety, the adsorbed stabilizing layers on the dispersed particles cannot interpenetrate each other when the particles collide. This reduces the number of configurations available to the adsorbed stabilizing tails, resulting in a negative entropy change and positive ΔG. On the other hand, if the dispersion medium is a poor solvent, the adsorbed layers on the particles may interpenetrate thermodynamically and induces particles agglomeration.

concept that was first introduced by Edwards et al. [54]. The porous particles include hollow porous particle [42] and porous nanoparticle-aggregate particles (PNAPs) [14]. Unfortunately, most of the work has been focused on microsuspension or polymeric colloidal formulations and has not been applied to pure drug nanoparticles.

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Table 1 summarizes a few published studies on pharmaceutical nanosuspensions. Due to the vast amount of literature work on the pharmaceutical nanosuspensions, this review will focus only on the studies that provide a more profound enlightenment on the stabilizer selection for nanosuspensions. The summary table shows that most of nanosuspensions were generated in aqueous medium, with only a limited number of nanosuspensions made in non-aqueous environment. The commonly used ionic stabilizers in aqueous medium include sodium dodecyl sulfate (SDS), sodium lauryl sulfate (SLS), lecithin and docusate sodium. The non-ionic surfactants used in aqueous medium are usually selected from Pluronic® surfactants, Tween 80, polyethylene glycol (PEG), polyvinyl alcohol (PVA) polyvinylpyrrolidone (PVP) and cellulose polymers such as hydroxypropyl cellulose (HPC) and hydroxypropyl methylcellulose (HPMC).

The stabilizers are not only used to provide short- and long-term storage stability for nanosuspensions, but also to achieve successful formation and stabilization of nanocrystals during particle production. Lee et al. designed and synthesized various amino acid copolymers containing lysine as the hydrophilic segments with alanine, phenylalanine or leucine as hydrophobic moieties [49]. Wet comminution was used to produce naproxen nanosuspensions in presence of HPC and amino acid copolymers. Lysine copolymer with alanine was unable to produce submicron particles while the other copolymers with phenylalanine and leucine were capable of forming the nanoparticles. The size of nanocrystals was proven to be constant over 1 month storage and the crystallinity was also shown to be preserved after the wet comminution process. Furthermore, hydrophobicity of the copolymers was identified as the key factor in achieving the stable nanosuspensions, attributed to strong polymer adsorption onto the hydrophobic drug surfaces. Although this work did not provide an in-depth discussion on how the copolymers interacted with the drug nanoparticles, it illustrated the importance of careful selection of the anchor group (that is attached to the drug surface) in facilitating the production of a stable nanosuspesion. In the subsequent study [45], they attempted to understand the nature of interactions between polymeric stabilizers and drugs with different surface energies. Nanocrystals of seven model drugs with PVP K30 and HPC as stabilizers were generated using wet comminution. It was expected that a close match of surface energy between the stabilizers and drug crystals would promote the absorption of stabilizers onto drug particles, and thus help in reducing the particle size during the wet comminution process. Although surface energy did not seem to correlate well with particle size for HPC stabilized system, some trend was observed for PVP stabilized suspension with only one exception.

A further study with seven stabilizers (non-ionic stabilizers: HPC, PVP K30, Pluronic® F127 & F68, PEG and ionic stabilizers: SDS and benzethoinum chloride) and eleven model drugs was conducted by the same group in order to provide more understanding on the stabilization mechanism [48]. Again, the general trend between surface energy and particle size reduction was not observed in this work. PEG was unsuccessful in reducing the particle size of most drug candidates while the other non-ionic stabilizers proved to be effective in reducing the size of five drug candidates that had similar surface energies to the stabilizers. F68 was shown to be the most effective stabilizer (successfully stabilizing nine drug candidates), which could be due to its strong chain adsorption onto the drug crystals through the hydrophobic polypropylene glycol (PPG) units. F127 was found to be less efficient than F68 likely because the short processing time led to inefficient physical adsorption of higher molecular weight F127 to the drug surface. This study demonstrated that a combination of ionic and non-ionic stabilizers is not always beneficial to enhance stabilization, A few combinations of SDS or benzethoinum chloride 374 with various non-ionic stabilizers resulted in positive stability effects 375 while the others did not. The effects of physicochemical properties of 376 the drugs on the stabilization were also explored in this study. In 377 general, drugs with lower aqueous solubility, higher molecular weight 378 and higher melting point were shown to have higher chance for 379 successful nanosuspension formation.

Van Eerdenbrugh et al. conducted an expanded study using 13 381 stabilizers at 3 different concentrations to stabilize 9 drug compounds 382 [47]. The particles were generated using the wet milling technique. 383 The success rate in producing nanosuspensions using polysaccharide 384 based stabilizers [HPMC, methylcellulose (MC), hydroxyethylcellu- 385 lose (HEC), HPC, carboxymethylcellulose sodium (NaCMC), alginic 386 acid sodium (NaAlg)] was limited by the high viscosity of these 387 polymeric stabilizer solutions. Increasing concentration of these 388 stabilizers did not appear to be helpful. In contrast, the other 389 stabilizers [PVP K30, PVP K90, PVA, Pluronic® F68, polyvinyl 390 alcohol-polyethylene glycol graft copolymer (K-IR), Tween 80 and 391 D-α-tocopherol polyethylene glycol 1000 succinate (TPGS)] did not 392 encounter the viscosity issue, PVA was ineffective in producing the 393 nanosuspension and the success probability of PVP K30, PVP K90, F68 394 and K-IR is highly dependent on their concentration. Higher 395 concentrations (25 wt.% and 100 wt.%) increased the stabilizing 396 efficacy significantly. Tween 80 and TGPS were proven to be most 397 effective stabilizers. Addition of TGPS (at concentrations >25 wt.%) 398 allowed nanosuspension formation for all tested drug compounds. No. 399 correlation was observed between drug physicochemical properties 400 (molecular weight, melting point, log p, solubility and density) and 401 nanosuspension formation success rate. It was demonstrated that 402 surface hydrophobicity of the drug candidates was the driving force 403 for nanoparticles agglomeration, thus lowering the success rate of 404 nanosuspension production.

Mishra et al. explored nanosuspension stability issues during both 406 production and storage [29]. Hesperetin nanosuspensions were 407 produced using HPH with Pluronic® F68, alkyl polyglycoside 408 (Plantacare 2000) and inulin lauryl carbamate (Inutec SP1), or 409 Tween 80 as stabilizers. It was demonstrated that all stabilizers 410 were suitable for successful production of hesperetin nanosuspen- 411 sions. The size of nanocrystals was dependent on power density 412 applied in the homogenization process and the hardness of the 413 crystals. The effect of stabilizers on the particle size was negligible. 414 Short-term stability over a period of 30 days was examined in order to 415 evaluate the stabilizer efficiency. ZP was measured as a key parameter 416 to predict the stability. In distilled water, the ZP values of all the 417 nanosuspensions fell between -30 and -50 mV and the values 418 dropped significantly in the original dispersion medium. This can be 419 explained by the fact that adsorbed layers of large molecules shifted 420 the shear plane to a longer distance from the particle surface, thus 421 reducing the measured value of zeta potential (Fig. 4). However, the 422 low ZP value does not point to an unstable suspension in this case, 423 which could be due to the additional presence of steric stabilization 424 mechanism. Both Inutec and Plantacare stabilized nanosuspensions 425 also showed significant reduction of ZP measured from water to 426 dispersion medium, indicating a thick absorbed steric layer and good 427 stability. F68 exhibited only slight decrease in ZP, indicating a 428 relatively thin stabilization layer. The ZP value of Tween 80 was 429 only -13 mv in the dispersion medium, pointing to a potentially 430 problematic stabilization. The study demonstrated that zeta potential 431 measurement is a good predictor for storage stability. Nanosuspen- 432 sions stabilized by Inutec and Plantacare were stable at all storage 433 conditions (4, 25 and 40 °C) up to 30 days while F68 stabilized 434 nanosuspensions were shown to be less stable. The Tween 80 435 formulation stability was the poorest. Pardeike et al. [30] conducted 436 a similar study using phospholipase A2 inhibitor PX-18 nanosuspen- 437 sions produced by HPH with Tween 80 as stabilizer. In this work, ZP of 438 the homogenized nanosuspensions was dropped from -50 mV to 439

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Literature summary of pharmaceutical nanosuspensions.

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]	Nanoparticles compound	Manufacturing technique	Delivery route	Dispersion medium	Stabilizers	Reference
(Oridonin	НРН	NA	Water	PVP K25, Brij 78, SDS, Pluronic@ F68, lecithin	Gao et al. (2007) [55]
(Oridonin	нрн	IV	Water	Pluronic® F68, lecithin	Gao et al. (2008) [56]
- 1	Budesonide	нрн	Inhalation	Water	Lecithin, Span 85, tyloxapol, cetyl alcohol	Jacobs et al. (2002) [57]
- 1	Buparvaguone	нрн	Inhalation	Water	Pluronic® F68 and PVA	Hernadez-Trejo et al.(2005) [58]
	Buparvaguone	НРН	Oral	Water	Pluronic® F68 and lecithin	Jacobs et al. (2002) [59]
	Diclofenac acid	нрн	Oral	Water	Pluronic® F68	Lai et al. (2009) [60]
	Azothromycin	нен	NA	Water	Lecithin, Pluronic® F68, Tween 80	
	_					Zhang et al. (2007) [61]
	Rutin	нрн	Oral	Water	SDS	Mauludin et al. (2009) [62]
	Rutin	НРН	Oral	Water	SDS, Tween 80, Pluronic® F68, PVA	Mauludin et al. (2009) [63]
	Farazepide	нрн	NA	Water	Tween 80, Pluronic® F68	Jacobs et al. (2000) [64]
(Omeprazole	HPH	IV	Water	Pluronic® F68	Moschwitzer, (2004) [65]
- /	Amphotericin B	HPH	Oral	Water	Tween 80, Pluronic F68	Kayser et al. (2003) [22]
1	Nimodipine	нен	IV	Water	Pluronic@ F68, sodium cholic acid and mannitol	
	Albendazole	нен	Oral	Water	SLS, Carbopol, PS 80, hpmc	Kumar et al. (2008) [23]
	RMKP 22	нен	NA	Water	Phospholipon 90	Peters et al. (1999) [67]
					• •	
1	Hesperetin	НРН	Dermal	Water	Pluronic® F68, Inutec SP1, Tween 80 and Plantacare 2000	Mishra et al. (2009) 29
ŀ	Hydrocortisone, prednisolone and dexamethasone	нрн	Opthalmic	Water	Pluronic® F68	Kassem et al. (2007) 68
1	Ascorbyl palmitate	НРН	NA	Water	SDS, Tween 80	Teeranachaideekul et (2008) [6
	RMKK99	нрн	NA	Water	Potassium oleate, Tween 80	Krause et al. (2001) [70]
	Nifedipine	нрн	NA	Water	HPMC	Hecq et al. (2005) [71]
	Indisclosed	нрн	Oral	Water	SLS, HPMC, PVA, Acaciae Gum, Pluronic® F127	
						Hecq et al. (2006) [72]
	Hydroxycamptothecin	НРН	NA	Water	Lipoid S75, Pluronic® F68, Solutol® HS 15	Zhao et al. (2010) [73]
	Asulacrine	нрн	IV	Water	Pluronic® F68	Ganta et al. (2009) 74
	RMKP 22	нрн	NA	Water	Tween 80	Muller et al. (1998) [75]
F	RMKP 22	нрн	NA	Water	Tween 80, Glycerol	Grau et al. (2000) [76]
F	X-18	HPH	NA	Water	Tween 80	Pardeike et al. (2010) [30]
F	X-18	НРН	NA	Water	Tween 80	Wang et al. (2010) [77]
	ilybin	НРН	Oral, IV	Water	Lecithin, Poloxamer 188	Wang et al. (2010) [78]
	arazepide	НРН	IV	Water	Pluronic® F68, Tween 80, Glycerol	
						Jacobs et al. (2000) [64]
	Omeprazole, albendazole and danazol	Wet milling	Oral	Water	Pluronic® F108, F68	Tanaka et al. (2009) [79]
F	luticasone, budesonide	Wet milling	Inhalation	Water	Tween 80	Yang et al. (2008) [80]
	Naproxen	Wet milling	NA	Water	HPC, arginie hydrochloride	Ain-Ai et al. (2008) [81]
	oviride	Wet milling	NA	Water	Tween 80, Pluronic® F68	Van Eerdenbrugh et al. (2007)
		_				
	line different compounds	Wet milling	NA	Water	13 different stabilizers	Van Eerdenbrugh et al. (2009)
	linc Insulin	Wet milling	NA	Water	Pluronic® F68, sodium deoxycholate	Merisko-Liversidge et al. (2004)
E	thyl Diatrizoate	Wet milling	NA	Water	Poloxamine 908	Na et al. (1999) 84
C	innarizine, itraconazole and phenylbutazone	Wet milling	NA	Water	TPGS 1000	Van Eerdenbrugh et al. (2008)
1	line different compounds	Wet milling	NA	Water	TPGS 1000	Van Eerdenbrugh et al. (2008)
	Beclomethasone dipropionate	Wet milling	Inhalation	Water	PVA	Wiedmann et al. (1997) [87]
	dipivirine	Wet milling	Parenteral	Water	Pluronic® F108, TPGS 1000	
	•	_			-	Baert et al. (2009) [88]
	Indisclosed	Wet milling	NA	Water	Plasdone S-630, docusate sodium	Deng et al. (2008) [89]
F	iposulfan, etoposide, camptothecin, paclitaxel	Wet milling	NA	Water	Tween 80, Span 80, Pluronic® F108, F127	Merisko-Liversidge et al. (1996)
N	laproxen	Wet comminution	NA	Water	Copolymers of amino acids	Lee et al. (2005) [49]
	even different compounds	Wet comminution	NA	Water	HPC, PVP	Choi et al. (2005) [45]
	leven different compounds	Wet comminution	NA	Water	HPC, PVP, PEG, SDS, Pluronic® F68, F127,	Lee et al. (2008) [48]
					benzethonium chloride	
0	ihydroartemisinin	Vibrational rod milling	NA	Water	PVP K30, sodium deoxycholate	Chingunpitak et al.(2008) [91]
	robucol	Vibrational rod milling	NA	Water	PVP, SDS	Pongpeerapat et al. (2008) [92]
			NA	Water	SLS, PVP K30, Pluronic® F68, F127,	
41	buprofen	Precipitation, microfluidization	17/1	***************************************	Tween 80, HPMC	Verma et al. (2009) [31]
۲	lydrocortisone	Precipitation. microfluidization	NA	Water	PVP, HPMC, SLS	Ali et al. (2009) [93]
11	buprofen	Solvent diffusion, melt emulsification	NA	Water	PVA, PVP K25, Pluronic® F68, Tween 80,	Kocbek et al. (2006) [94]
A	dendronate-gallium, alendronate-gadolinium	Complex precipitation	NA	Water	None	Epstein et al. (2007) [95]
P	aclitaxel	Stabilization of nanocrystal (SNC)	NA	Water	Pluronic® F127	Deng et al. (2010) [50]
F	elodipine	Antisolvent precipitation & Wet-milling	NA	Water	PVP K30, SDS, docusate sodium	Lindfors (2007) [96]
٨	laproxen	Antisolvent precipitation	Oral	Water	PVP K15, Pluronic@ F127	Chen et al. (2009) [97]
		Antisolvent precipitation	NA .	Water		
	arbamazepine	• •			HPMC, PVP K17	Douroumis et al. (2007) [98]
	yclosporin A	Antisolvent precipitation	Inhalation	Water	Tween 80	Tam et al. (2008) [99]
	Indisclosed	Antisolvent precipitation, Wet milling		Water	PVP, SDS, Miglyol, docusate sodium	Sigfridsson et al. (2007) [100]
В	-methasone valerate-17, oxcarbazepine	Antisolvent precipitation		Water	HPMC, lipoid S75, PEG-5 soy sterol	Douroumis et al. (2006) [101]
	etinoic acid	Antisolvent precipitation	NA	Water	None	Zhang et al. (2006) [102]

Table 1	(rontinued)	

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4	Nanoparticles compound	Manufacturing technique	Delivery route	Dispersion m ed ium	Stabilizers	Reference
,	2-devinyl-2-(1-hexyloxyethyl) pyropheophorbide	Antisolvent precipitation	NA	Water	None	Baba et al. (2007) 103
3	Nitrendipine	Precipitation— ultrasonication	Oral	Water	PVA	Xia et al. (2010) 104
7	Indomethancin	Emulsion diffusion	NA	Water	Cyclodextrins	Makhlof et al. (2008) [52]
3	Celecoxib	Emulsion diffusion	Oral	Water	Tween 80, PVP K30, SDS	Dolenc et al. (2009) [105]
9	Griseofulvin	Emulsion diffusion	NA	Water	Tween 80, Oramix CG-110	Trotta el al.(2003) [106]
)	Mitotane	Emulsion diffusion	NA	Water	Tween 80, caprylyl-capryl glucoside, lecithin	Trotta el al.(2001) [107]
ı	Griseofulvin	Microemulsion diffusion	NA	Water	Lecithin	Trotta el al.(2003) [108]
2	Lysozyme	Emulsification/freeze- drying	Inhalation	HFA	None	Nyambura et al.(2009) 109
3	Bovine serum albumin	Thin film freezing	Inhalation	HFA	None	Engstrom et al.(2009) [41]
ı	Itraconazole	Thin film freezing	Inhalation	HFA	None	Tam et al.(2010) [40]
5	Insulin	Emulsification + freeze-drying	Inhalation	HFA	Citral, cineole	Nyambura et al.(2009) [110]
6	Salbutamol sulfate	Microemulsion + freeze-drying	Inhalation	HFA	Lecithin, docusate sodium	Dickinson et al. (2001) [111]
7	Salbutamol sulfate	HPH	NA	Acetonltrile	Tween 80	Ahmad et al. (2009) [112]
8	Horseradish peroxidase, carbonic anhydrase, lysozyme, subtilisin carlsberg and α-chymotrypsin	Freeze-drying	NA	Ethyl acetate	Methyl-&-cyclodextrin	Montalvo et al. (2008) [113]
Ð	Diclofenac	Emulsification + freeze drying	Transdermal	lsopropyl myristate	Sucrose ester	Piao et al. (2007) 114

around -20 mV when tested from water to dispersion medium. It is generally believed that ZP of ± 20 mV is sufficient to maintain a stable formulation with a combined electrostatic and steric stabilization [30]. The PX-18 nanosuspension was shown to be physically stable (no changes in particle size distribution) for more than half year at the storage condition of 5 and 25 °C. However, physical instability was observed after 1 month storage at a higher storage temperature. This could be due to the decreased dynamic viscosity and enhanced diffusion constant at higher temperature.

There is another interesting work by Pongpeerapat et al. investigating probucol/PVP/SDS ternary ground mixture (GM) that was prepared with a vibrational rod mill [92]. The produced primary probutcol nanoparticles were around 20 nm in presence of both SDS and PVP. An interesting phenomenon was observed following the dispersion of the GM into water. For GM stabilized with PVP K17 and SDS, spherical agglomerates of primary nanocrystals were formed immediately in the size of around 90 nm after dispersion of the GM into water. A further agglomeration to around 160 nm in size occurred gradually during the storage stability study. In the case of PVP K12 and SDS, agglomerations of approximately 180 nm were observed after 4 days of storage and then remained stable up to 84 days. This phenomenon is illustrated in Fig. 5. Above critical aggregation concentration, SDS complexes with PVP to form a "necklace" structure in aqueous medium through both electrostatic and hydrophobic interactions. Following dispersion of probucol/PVP K17/SDS into water, PVP K17/SDS "necklace" complex interacted with primary 465 drug nanoparticles, causing immediate agglomeration of the primary 466 nanoparticles into 90 nm aggregates. The 160 nm secondary nano-467 particles were formed due to further gradual agglomeration process. 468 The stabilization of probucol nanocrystals was attributed to formation 469 of PVP K17/SDS layered structure on the surface of probucol. For the 470 GM of probucol/PVP K12/SDS, agglomeration of primary drug 471 nanoparticles occurred more rapidly because of the insufficient 472 surface coverage of PVP K12 and SDS on the probucol surface. 473 Stabilization of the nanosuspension was linked to absorption of PVP 474 K12 on the surface of probucol nanocrystals, owing to the absence of 475 layered structure.

Despite the proven importance of stabilizers in preventing particle 477 agglomeration, there have been a few studies that generated stable 478 nanosuspensions without stabilizers. Baba et al. prepared 2-devinyl-2-(1-hexyloxyethyl)pyropheophorbide (HPPH) nanosuspensions 480 without any stabilizer and reported formulation stability for more 481 than 3 months (103). The self-stabilization of the nanosuspensions 482 was attributed to a high ZP value (—40 mv) resulting from the 483 deprotonation of the carboxylic end group of HPPH molecules. A 484 similar self-stabilized nanosuspension was reported in another study 485 in which amorphous all-trans retinoic acid nanoparticles were shown 486 to be stable in aqueous medium up to 6 months. Epstein et al. [95] 487 prepared self-suspended alendronate nanosuspensions by combining 488 the negative charged alendromnic acid with gallium (Ga) or 489

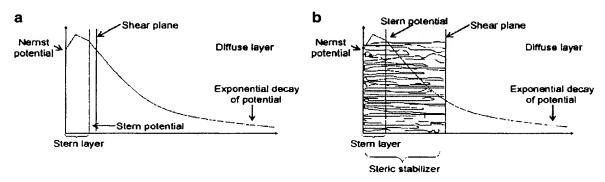


Fig. 4. Location of shear plane in an electrostatic stabilized system (a) and in a combined steric-electrostatic stabilized system (b). Reprinted from Ref. [30] with permission from ELSEVIER.

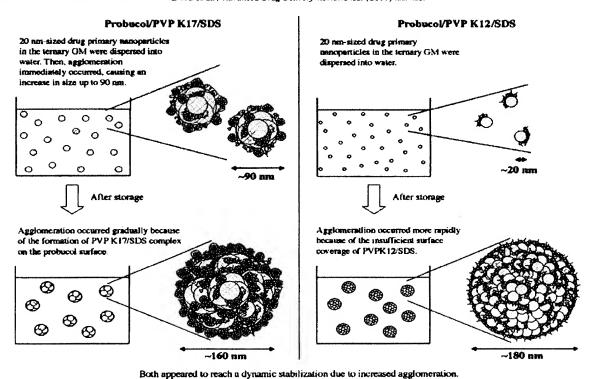


Fig. 5. Schematic overview of agglomeration/stabilization mechanism of probucol/PVP/SDS ternary ground mixture after dispersion into water. Reprinted from Ref. [92] with permission from ELSEVIER.

gadolinium (Gd) under sonication as complex nanoparticles. The alendronate-Ga nanosuspension was shown to be stable for more than 3 months, while the alendronate-Gd nanosuspension was stable for only 3 days. These stability profiles correlated well with their ZP values (33 mV for Ga complex vs. 21 mV for Gd complex).

2.2.3. Crystal growth

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Crystal growth in colloidal suspensions is generally known as Ostwald ripening and is responsible for changes in particle size and size distribution. Oswald ripening is originated from particles solubility dependence on their size. Small particles have higher saturation solubility than larger ones according to Ostwald-Freundlich equation [115], creating a drug concentration gradient between the small and large particles. As a consequence, molecules diffuse from the higher concentration surrounding small particles to areas around larger particles with lower drug concentration. This generates supersaturated solution around the large particles, leading to drug crystallization onto the large particles. This diffusion process leaves an unsaturated solution surrounding the small particles, causing dissolution of the drug molecules from the small particles into the bulk medium. This diffusion process continues until all the small particles are dissolved. The Ostwald ripening is essentially a process where large particles grow at the expense of smaller particles [36.37], which subsequently leads to a shift in the particle size and size distribution of the colloidal suspension to a higher range. The diffusion and crystal growth during Ostwald ripening is shown schematically in Fig. 6.

A narrow particle size distribution can minimize the saturation solubility difference and drug concentration gradients within the medium, and thus help to inhibit occurrence of the Ostwald ripening [37]. This can perhaps explain why Ostwald ripening is not a major concern for nanosuspensions with uniform particle size [10,20]. Stabilizers may also alleviate Ostwald ripening as long as they do not enhance the drug solubility [116.117]. Being absorbed on the

nanoparticles surface, the stabilizers can reduce the interfacial tension 522 between the solid particles and liquid medium, and thus preventing 523 the Ostwald ripening. Solubility, temperature, and mechanical 524 agitation also affect Ostwald ripening [117]. Verma et al. produced 525 ibuprofen nanosuspensions by microfluidization milling with the aid 526 of various stabilizers (HPMC, Pluronic® F68 & F127, Kollidon 30, SLS) 527 [31]. The particle size obtained with microfluidization showed some 528 correlation with the ibuprofen solubility in aqueous stabilizer 529 solutions. A higher solubility of ibuprofen in the solution of SLS, 530 Tween 80 and Pluronic® F127 resulted in larger particles due to 531 Ostwald ripening that occurred during process. A similar correlation 532 was observed for ibuprofen particles during storage where Ostwald 533 ripening was also believed to the driving factor for formation of larger 534 particles. Van Eerdenbrugh et al. demonstrated that Ostwald ripening 535 was highly dependent on temperature by exploring TPGS stabilized 536 nanosuspensions for 9 different drug candidates [86]. Following 537 3 months storage at room temperature, Ostwald ripening occurred in 538 8 out of 9 nanosuspensions studied. Enhanced Ostwald ripening was 539 observed at 40 °C storage, while lowering temperature to 4 °C slowed 540 down or even stopped Ostwald ripening effects.

2.2.4. Change of crystalline state

Crystalline state is one of the most important parameters affecting 543 drug stability, solubility, dissolution and efficacy. The main issue with 544 crystalline state change is the transformation between amorphous 545 and crystalline state. The high energy top-down manufacturing 546 techniques tend to create partially amorphous nanosuspensions and 547 some bottom-up techniques can create completely amorphous 548 particles. The high energy amorphous particles are unstable and 549 inclined to convert to low energy crystalline state over time. This 550 conversion occurs depending on different parameters, such as 551 temperature, dispersion medium, stabilizers and the presence of 552 crystalline particles. Lindfors et al. produced Felodipine amorphous 553

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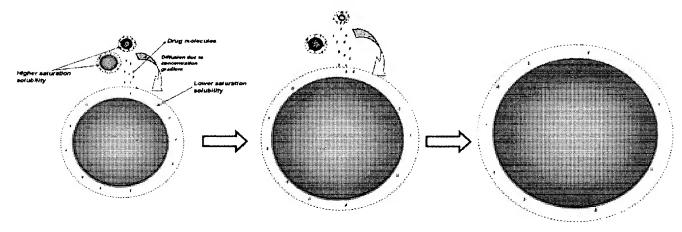


Fig. 6. Schematic illustration of Ostwald ripening.

nanosuspensions via anti-solvent precipitation under sonication [96]. They demonstrated that amorphous nanoparticles were highly unstable in the presence of small amounts of crystalline particles. This was attributed to saturation solubility differences between amorphous and crystalline nanoparticles that initiated a similar diffusion process to Ostwald ripening, leading to a rapid conversion of amorphous nanoparticles to crystalline state. Although most of amorphous particles have been shown to be unstable, a few amorphous nanosuspensions have been demonstrated to be stable over a certain period of time. Amorphous hydrocortisone nanosuspensions, produced through a bottom-up nanoprecipitation technique using microfluidic reactors, was found to remain stable after 3 months storage at room temperature [93]. Amorphous all-trans retinoic acid nanosuspensions, prepared by an anti-solvent precipitation technique, were also shown to be stable over 6 months storage at 4 °C [102].

Manufacturing process might also induce some other type of crystalline transformation. Lai et al. prepared the diclofenac acid (DCF) nanosuspensions by HPH with two different crystalline forms (DCF1 and DCF2) [60]. 5 w/w% Pluronic® F68 was used as a stabilizer. XRD analysis showed that these two crystalline forms belonged to the same polymorph with differences in molecular conformation and crystal size. It was demonstrated that the HPH process caused the partial transformation of DCF2 to DCF1 while no effect on DCF1 was observed. The change in the crystalline structure was attributed to the solubilization of DCF2 during HPH process and its subsequent recrystallization as the DCF1 form.

2.2.5. Stability issues with solidification process of nanosuspensions

When stable nanosuspensions are unattainable, the solid dosage form is the ultimate solution. The most common solidification processes are freeze drying and spray drying [10,19.20,118]. Since most solidified nanoparticle dry powders are usually reconstituted back into nanosuspensions during administration, drug nanocrystal growth or agglomeration during drying process needs to be prevented in order to maintain the nanosizing features such as rapid dissolution following the reconstitution. Adding matrix formers, such as mannitol, sucrose and cellulose, into nanosuspensions prior to drying is the common approach to overcome the stability issues during solidification process [19]. Since several excellent reviews have been published on this topic [19,25,118], the readers are directed to those reviews for more details.

2.2.6. Chemical stability

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Since drug nanocrystals are usually dispersed in nanosuspensions with a limited solubility, the possibility of chemical reactions is not as substantial as that in solution-based formulations. Consequently,

chemical stability of nanosuspensions is generally superior to that of 598 solutions. Paclitaxel serves as a good example to illustrate this [119]. 599 Fig. 7(a) shows an HPLC diagram of paclitaxel nanosuspensions 600 stabilized with Pluronic® F68 after 4 years of storage at 4-8 °C. No 601 visible degradation product was observed with a recovery of more 602 than 99%. On the other hand, paclitaxel solution with methanol as 603 cosolvent showed clear degradation only after 48 h at room 604 temperature (Fig. 7(b)). The excellent chemical stability of paclitaxel 605 nanosuspensions was attributed to a mechanism similar to oxidized 606 layer on the aluminum surface. Monolayer degradation on the 607 nanocrystals surface was created once they were exposed to water 608 and oxygen, as illustrated in Fig. 7(c). This monolayer could protect 609 the inner part of drug crystals from further degradation, and thus 610 enhance chemical stability of the nanosuspensions.

Unlike the physical stability issue that is a common concern for 612 nanosuspensions, chemical stability is drug specific. Each molecule 613 has its particular functional groups and reaction mechanism that 614 affects the stability. For example, chemical functionalities, such as 615 ester and amides, are susceptible to hydrolytic degradation, while 616 amino groups may undergo oxidative degradation [120]. Although 617 chemical stability of nanosuspensions is usually not a major concern, 618 extra attention should be paid to drug molecules with solubility 619 greater than 1 mg/mL or with low concentration in suspension [120]. 620 The common strategy to enhance the chemical stability is to transform 621 the nanosupensions into dry solid dosage form which is much more 622 stable than nanosuspensions [19] or to increase the concentration of 623 the nanosuspensions [120].

2.3. Additional stability issues relate to large biomolecules

Large biomolecules discussed in this review are mainly referred to 626 therapeutic protein and peptide. The molecular structure of protein/ 627 peptide is distinctly different and more complicated as compared to 628 that of the small molecules. The structures of large molecules are 629 generally differentiated into four structures, i.e. primary, secondary, 630 tertiary and quaternary structures [34]. These different structures 631 refer to the sequence of the different amino acids, regions where the 632 chains are organized into regular local structures by hydrogen 633 bonding such as alpha helix and beta sheet, the mechanisms on 634 how the protein/peptide chain folds Into a 3-dimensional conforma- 635 tion, and the composition of multiple protein/peptide molecules 636 assembly, respectively [32,33,123]. The intact molecular structure of 637 protein/peptide is essential to maintain their therapeutic efficacy 638 [35,121]. Common stability issues associated with protein/peptide 639 include deamidation, oxidation, acylation, unfolding, aggregation and 640 adsorption to surfaces [35,121]. These stability issues are affected by 641

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Fig. 7. (a) HPLC diagram of paclitaxel aqueous nanosuspensions stabilized with Pluronic® F6B; (b) HPLC diagram of paclitaxel solution (methanol: 10 ml, water: 5 ml, paclitaxel: 20.8 mg); (c) Schematic illustration of stabilization mechanism of paclitaxel nanosuspensions. Reprinted from Ref. [119] with permission from ELSEVIER.

temperature, solution pH, buffer ion, salt concentration, protein concentration, and added surfactants, with solution formulations being more susceptible to the influence from these factors than the suspension formulations [34,35,121]. Although suspension formulations or solid state of protein/peptide have enhanced stability due to their reduced molecular mobility, other stability issues may arise during particle formation or formulation process. For example, irreversible denaturation and aggregation upon reconstitution were often observed for dehydrated protein through freeze drying or spraydrying [125,126]. To prevent this, supplementary excipients such as bulking agents or surfactants are usually introduced during lyophilization [122].

The vulnerable structure of protein/peptide creates challenges for formulation development. Instead of using "naked" protein, the common strategy to prevent protein/peptide denaturation is to encapsulate the biomolecules with carrier such as liposome [123]. SLN [124] or polymeric materials [125,126]. In addition to improving the stability, protein/peptide encapsulation can enhance bioavailability and provide sustained therapeutic release [125-128]. There has been plenty of work reported on encapsulated protein/peptide nanoparticles but very scarce studies on pure protein/peptide nanoparticles. Gomez et al. produced bovine zinc insulin nanoparticles using an electrospray drying technique and reported retained biological activities of the particles [129]. By using HPH, Maschke et al. attempted to micronize insulin in the medium of Myglyol 812 [130]. The stability and bioactivity of the insulin were maintained in spite of the harsh HPH process conditions. Merisko-Liversidge et al. [83] also noticed retained stability and bioactivity of zinc-insulin nanosuspensions that were produced through a wet milling process in presence of Pluronic® F68 and sodium deoxycholate. Nyambura et al. utilized a bottom up technique (combination of emulsification and freeze drying) to generate insulin nanoparticles (80 w/w% insulin with 20 wt.% lactose) [110]. The particles were then dispersed into HFA134a to produce an MDI formulation. The molecular integrity of insulin formulation, measured by HPLC, size exclusion chromatography, circular dichroism and fluorescence spectroscopy, indicated that native structures (primary, secondary and tertiary) were retained after particle formation and formulation process. The presence of surfactant (lecithin) and lyoprotectant (lactose) was believed to be responsible for preservation of the insulin structures. In their follow up work [109], they applied a similar approach to produce composite

nanoparticles of lysozyme and lactose for MDI formulations. The 683 retained biological activity of lysozyme was enhanced with increasing 684 lactose concentration in the particles, and reached maximum (99% 685 retained activity) with 20 w/w% lactose. Nanoprecipitation coupled 686 with freeze drying was used as well in this work to produce spherical 687 nanoparticles containing 80 w/w% lysozyme with fully preserved 688 bioactivity. It was demonstrated that bioactivity of lysozyme 689 nanoparticles remained unchanged when in contact with HFA 134a, 690 Yu et al. compared the effectiveness of spray freezing into liquid (SFL) 691 and spray-freeze drying (SFD) processes in producing bioactive 692 lysozyme particles [131]. Both processes generated highly porous 693 micro-sized aggregates of lysozyme primary nanoparticles in the size 694 of 100-300 nm. SFL process was shown to produce lysozyme with 695 lower aggregation and higher enzyme activity as compared to the SFD 696 process, which was attributed to the shorter exposure time to the air- 697 water interface during the SFL atomization process. 698

3. Characterizing stability of drug nanoparticles and nanoparticle $\frac{699}{700}$

Selection of characterization techniques for drug nanoparticles 701 stability is dependent on the nature of stability issues and product 702 dosage form. A few commonly used stability characterization 703 techniques are listed in Table 2.

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3.1. Particle size, size distribution and morphology

Particle size and size distribution are the key parameters used for 706 evaluating the physical stability of nanoparticles. A variety of 707 techniques, including photon correlation spectroscopy (PCS), also 708 known as dynamic light scattering (DLS), laser diffraction (LD) and 709 coulter counter, are commonly used to measure the particle size and 710 size distribution (Table 2). The PCS/DLS is widely used to determine 711 the size and size distribution of small particles suspended in liquid 712 medium. The mean particle size and size distribution indicated as 713 polydispersity index (PDI) are the typical measured parameters of this 714 technique. A PDI value of 0.1 to 0.25 indicates a narrow size 715 distribution while a PDI greater than 0.5 refers to a broad distribution 716 [20]. Unfortunately, this technique is not capable of measuring size of 717 dry powders and its measurement range is too narrow (3 nm to 3 μ m) 718 to detect the interference from the microparticles (>3 μ m) within the 719

Table 2
Commonly used technique to evaluate the stability of nanoparticles,

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t2.3	Measured parameters	Techniques	Remarks
12.4	Particle size and size distribution	PCS/DLS	Pros: rapid, non-invasive.
t2.5			Cons: limited measurement range; apply only to liquid suspension.
t2.6		Laser diffraction	Pros: wide measurement range, rapid, non-invasive, apply to both liquid suspension and dry powder samples.
t2.7			Cons: particles are assumed to be spherical.
t2.8		Coulter counter	Pros: precise.
t2.9			Cons: apply only to spherical particles.
t2.10	Particle size and morphology	SEM/TEM	Pros: evaluate both particle morphology and size, very small quantity of sample required.
t2.11			Cons: challenging to acquire statistical size distribution, usually invasive, time-consuming,
t2.12		AFM	Pros: non-invasive, evaluate both particle morphology and size, very small quantity of sample required.
t2.13			Cons: challenging to acquire statistical size distribution, time-consuming.
t2.14	Sedimentation/creaming	Visual observation/laser backscattering/	-
		near infrared transmission	
t2.15	Particle surface charge/zeta potential	Laser Doppler electrophoresis	-
t2.16	Crystallinity state	XRD/DSC	-
t2.17	Chemical stability	HPLC/FTIR/NMR/MS	•

nanosuspensions. Therefore, LD is often used in combination with PCS to circumvent this issue. Laser diffraction has a much wider detection range (20 nm to 2000 μm) and it can be used to evaluate both suspension and dry powder samples. The typical LD characterization parameters are LD50, LD90 and LD99, indicating 50, 90 or 99% of the particles are below the given size, respectively. LD is especially suitable for characterizing parenteral and pulmonary suspensions due to it wide measurement range. LD can detect the presence of microparticles (>5 μm) which are detrimental to parenteral nanosuspensions. However, LD provides only relative size distribution. The Coulter counter, on the other hand, measures the absolute number of particles per volume unit for the different size classes, and is more precise than the LD.

Although PCS, LD and coulter counter techniques provide rapid measurement of particle size and size distribution, they do not have the capability in evaluating particle morphology. As direct visualization techniques, Scanning Electron Microscope (SEM), Transmission Electron microscope (TEM) and Atomic Force Microscope (AFM) are widely used for assessment of particle morphology. However, it is very challenging and time-consuming to measure a significant number of particles to achieve statistical size distribution using these techniques. In addition, they usually require additional sample preparation such as coating that could be invasive to the particles, potentially causing some changes in particle properties.

3.2. Sedimentation/creaming

The traditional method to evaluate sedimentation or creaming is by visual observation over a period of time. By measuring the volume of the settled or creamed particle layer relative to the total suspension volume within a specific time, a dimensionless parameter known as sedimentation or flocculation volume can be obtained as a quantitative evaluation of suspension stability. A higher flocculation volume indicates a more stable suspension. The structure of settled/creamed layer can be easily assessed by re-dispersing the suspension, i.e. easily re-dispersed suspension indicates loose flocs while a dense cake is hard to be broken by manual shaking. Other approaches to evaluate sedimentation/creaming include laser backscattering [132] and near-infrared transmission [133].

3.3. Particle surface charge

Laser Doppler electrophoresis is commonly used to measure ZP. This technique evaluates electrophoretic mobility of suspended particles in the medium. It is a general rule of thumb that an absolute

value of ZP above 60 mV yields excellent stability, while 30, 20 and 761 less than 5 mV generally results in good stability, acceptable short- 762 term stability and fast particle aggregation, respectively [29]. This rule 763 of thumb is only valid for pure electrostatic stabilization or in 764 combination with low-molecular weight surfactants, and is not valid 765 when higher molecular weight stabilizers are present [29].

3.4. Crystalline state

The crystallinity of drug nanoparticles is usually assessed by X-Ray 768 Diffraction (XRD) and/or Differential Scanning Calorimetry (DSC). 769 XRD differentiates amorphous and crystalline nanoparticles as well as 770 different polymorphic phases of the particles, while DSC is often used 771 as a supplementary tool to XRD. Crystalline particles usually have a 772 sharp melting peak which is absent in amorphous materials. The 773 melting point can also be utilized to differentiate different 774 polymorphs.

3.5. Chemical stability

HPLC is the most common characterization technique used to 777 evaluate chemical stability that provides precise quantitative analysis 778 on the degradation impurities. Mass spectrometry (MS) is often 779 coupled with HPLC to identify the molecular structure of impurities. 780 Some other techniques such as FTIR and NMR can also be used for 781 chemical stability assessment. However, they are not as precise and 782 sensitive as HPLC, and thus not widely used for stability assessment. 783

3.6. Additional techniques for assessing large biomolecule nanoparticle 784 and formulation stability 785

For large biomolecules, additional characterization tools are 786 generally required depending on the level of molecular structure to 787 be assessed. For instance, size exclusion chromatography and 788 electrophoresis are used to evaluate the primary structure of large 789 biomolecules, circular dichroism is to monitor the secondary and 790 tertiary structures while fluorescence spectroscopy is for tertiary 791 structure [34,134]. In addition, in-vitro bioassays or in-vivo efficacy 792 tests are needed to evaluate biological activities of the large 793 biomolecules, Insulin particles, as an example, have been tested for 794 its bioactivity either by in-vitro chondrocyte culture assays [130] or in-795 vivo monitoring of blood glucose level on rats following insulin 796 administration [83].

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4. Recommendations of general strategies for enhancing stability of nanoparticle formulations

Strategies to address different stability issues are usually tailored according to different aspects, such as therapeutic requirements, dosage form and manufacturing complexity. For example, as the particle size is reduced, the sedimentation rate is decreased so that the particles can stay suspended longer in nanosuspensions. The general wisdom is that the smaller the nanoparticles are, the better. Unfortunately, too small particles are not always desirable, as they may create undesired plasma peaks due to the significant increases in dissolution rate [28]. Moreover, manufacturing complexity may be increased as well when the particles size requirements become too stringent.

The use of stabilizers is the most commonly used technique in achieving a stable nanoparticle formulation. However, the stabilizer selection is known to be very challenging. The challenge stems mainly from two aspects: (i) lack of fundamental understanding of interactions within nanosuspensions and (ii) lack of an efficient and high throughput stabilizer screening technique. In the case of aqueous nanosuspensions, it is relatively easy to select stabilizers given that water-based stabilizing mojeties such as PEG and PVA are well known. However, selecting the anchor groups that interact strongly with the drug surface can be challenging due to the limited understanding on interactions between nanoparticles and stabilizers in molecular level. For non-aqueous nanosuspensions such as HFA-based MDI delivery system, understanding of solvation in the low-dielectric HFA medium is still in its infancy, which makes stabilizers selection even more challenging. Inefficient screening approaches are another hurdle for stabilizer selection. The current practice for stabilizer screening involves trial production of nanosuspensions with different stabilizers or stabilizer combinations, which could be burdensome and require vast amount of efforts especially with a large number of potential stabilizer candidates. AFM has recently been proven to be a feasible and efficient tool for stabilizer screening. Verma et al. demonstrated the feasibility of using AFM to select stabilizers for lbuprofen nanosuspensions [135]. The AFM measurements showed that HPMC and HPC had extensive surface absorption on the ibuprofen surface, as opposed to the inadequate surface absorption with PVP and Pluronic® surfactants. These results correlated well with their stabilizing performances in the nanosuspensions. This finding confirmed the significance of AFM in providing a scientific rationale for stabilizer selection and improving understanding of the stabilization mechanisms. Another technique, known as colloidal probe microscopy (CPM) which is derived from AFM, has also been widely used to study interactions between colloidal particles and is expected to be a useful tool for nanosuspension stabilizer screening [136].

Due to the significant challenges associated with stabilizer selection, self-stabilized nanosuspensions with no added stabilizer are highly desirable. This is not only for simplifying the formulation development process but also reducing stabilizer-based toxicity. Unfortunately, the challenges to engineer such self-suspended nanoparticles are tremendous with very few reported studies to date. A couple of approaches that could potentially be used to produce self-stabilized nanosuspensions include the creation of drug nanoparticles with high ZP and controlling morphology or surface properties of drug nanoparticles to minimize inter-particulate forces.

5. Conclusions

The stability of drug nanoparticles remains a very challenging issue during pharmaceutical product development. Stability is affected by various factors such as dosage form (nanosuspension vs. dry solid), dispersion medium (aqueous vs. non-aqueous), delivery route (oral, inhalation, IV or other routes), production technique (topdown vs. bottom-up) and nature of drug (small molecules vs. large

biomolecules). Despite the significant challenges associated with 861 stabilizer screening, adding a stabilizer or combination of stabilizers is 862 still the most commonly used and preferred approach to enhance the 863 stability of nanosuspensions. Further understanding of particle- 864 particle interactions within nanosuspensions and development of 865 high-throughput stabilizer screening tools are essential to facilitate 866 efficient stabilizer selection. Development of self-stabilized nanosus- 867 pensions, although currently seen as very complicated and challeng- 868 ing, is expected to grow with the continuing advancement in the field 869 of particle engineering. 870

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